

# Multiplexing Single-Vial Process Analytical Technologies

Through Vial Impedance Spectroscopy (TVIS)  
*and*  
Thermocouple Temperature Sensors

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[www.dmu.ac.uk/tvis](http://www.dmu.ac.uk/tvis)



FREEZE  
DRYING OF  
PHARMACEUTICALS  
& BIOLOGICALS

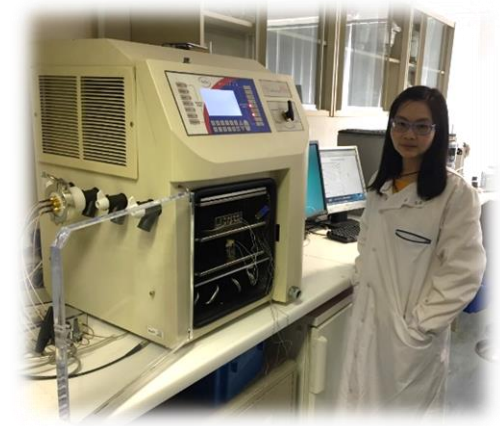
SHORT COURSE AND CONFERENCE

September 18 –21, 2018  
Dorint Hotel  
Garmisch-Partenkirchen, Germany

# Outline



- Description of TVIS measurement system
- Multiplexing
- Dual-electrode system and its applications
  - Ice region specific temperature prediction ( $T_i$ ,  $T_b$ )
  - Drying rate determination
  - Heat transfer coefficient ( $K_v$ ) determination
- Acknowledgements
- TVIS dielectric loss mechanisms



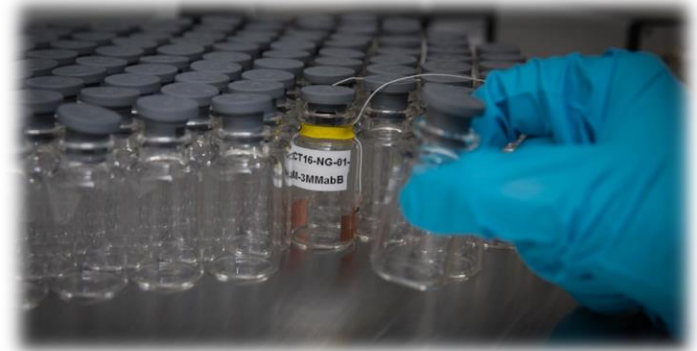
# Through Vial Impedance Spectroscopy (TVIS)

## *Description of Measurement System*

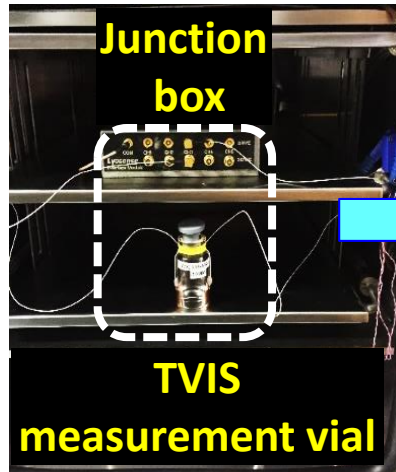
# Introduction to the TVIS System



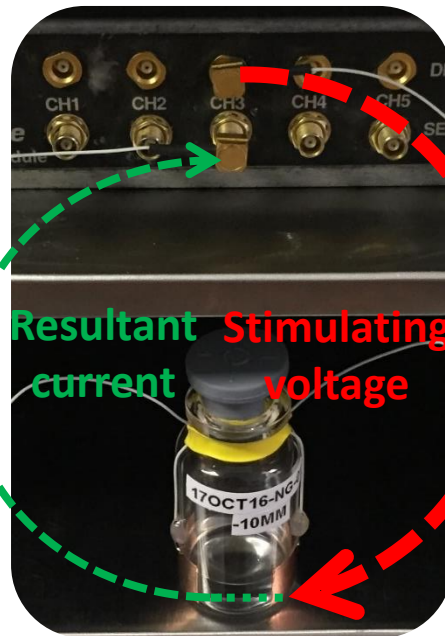
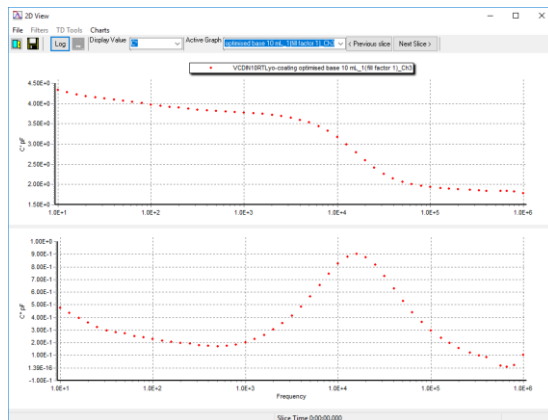
- Impedance spectroscopy characterizes the ability of materials to conduct electricity under an applied an oscillating voltage (of varying frequency)
- Impedance measurements **across a vial** rather than **within the vial**
- Hence **“Through Vial Impedance Spectroscopy”**
- Features
  - Single vial “non-product invasive”
  - Both freezing and drying characterised in a single technique
  - Non-perturbing to the packing of vials
  - Stopper mechanism unaffected



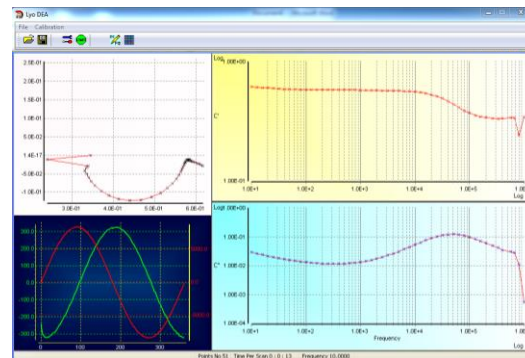
## Freeze drying chamber



## LyoView™ analysis software

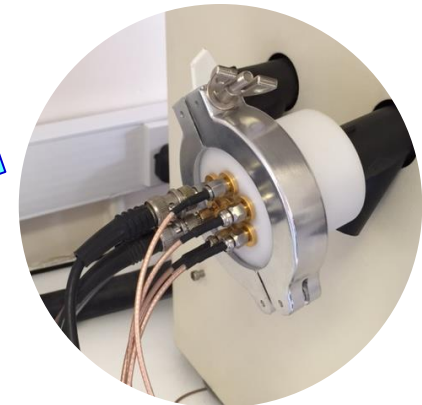


## LyoDEA™ measurement software



**TVIS**

## Pass-through



## TVIS system (I to V convertor)



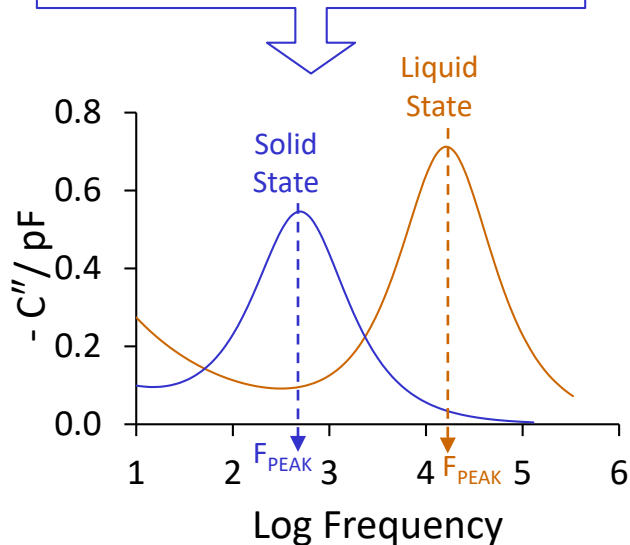
# Through Vial Impedance Spectroscopy (TVIS)

## *Applications*

# Through Vial Impedance Spectroscopy (TVIS)



Monitoring **Phase Behaviour**  
(ice nucleation temperature  
and solidification end points  
by using  $F_{PEAK}$ )

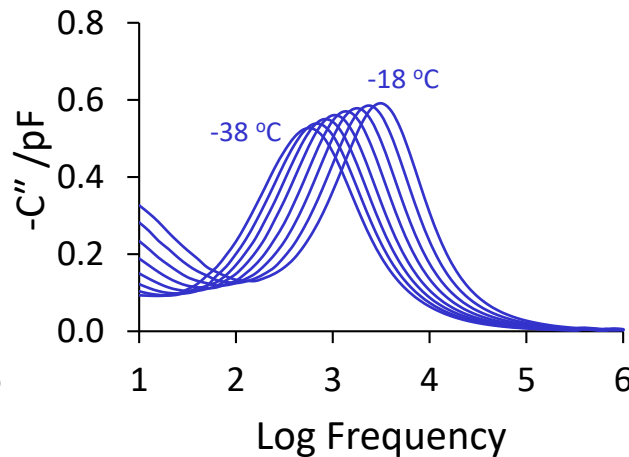
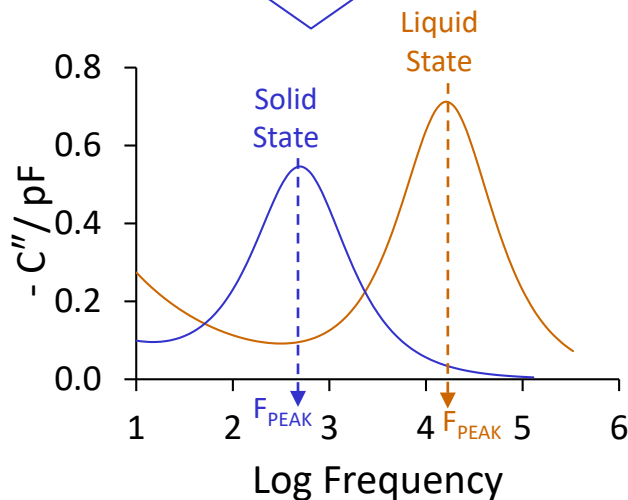


# Through Vial Impedance Spectroscopy (TVIS)



Monitoring **Phase Behaviour**  
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$F_{PEAK}$  temperature calibration  
for **predicting temperature** of  
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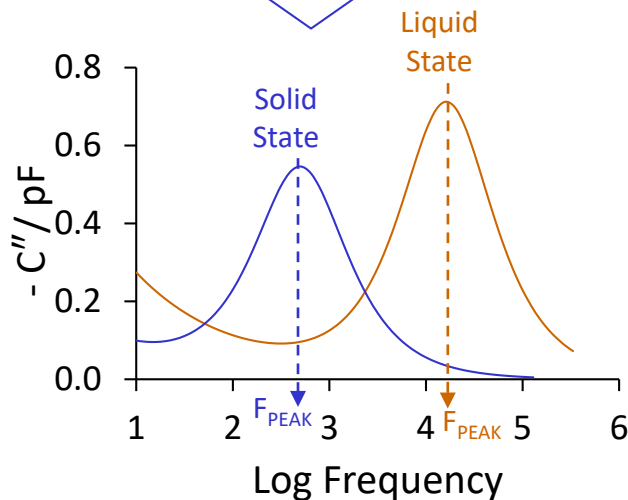




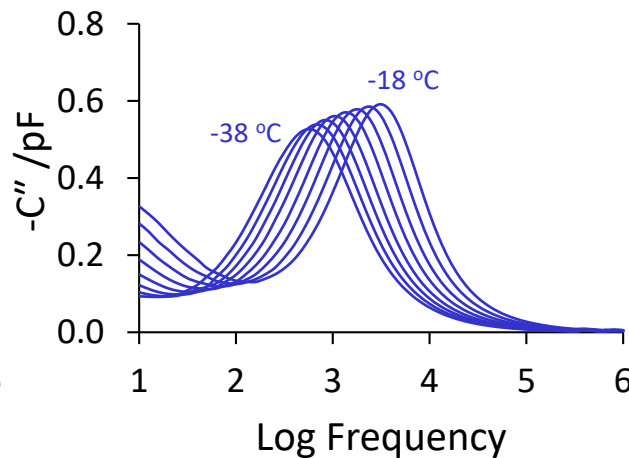
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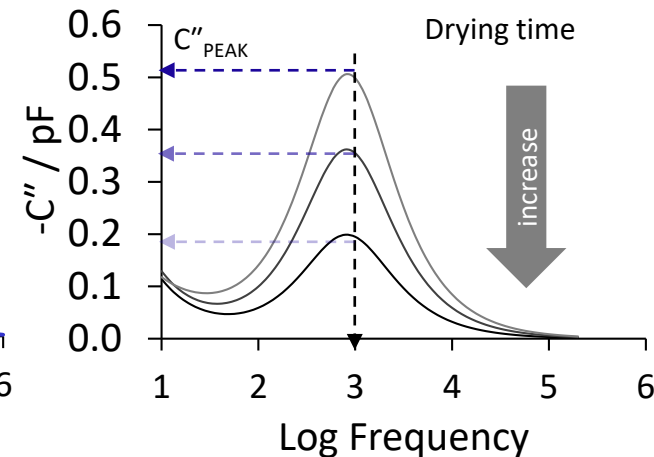
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$F_{PEAK}$  temperature calibration  
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Surrogate **drying rate**  
(from  $\frac{dC''_{PEAK}}{dt}$ )



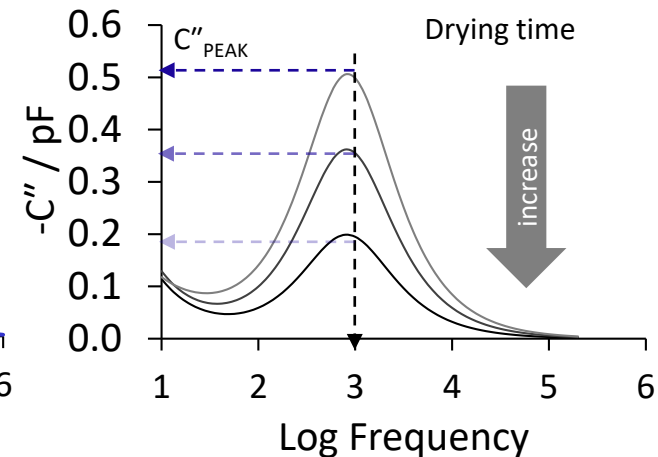
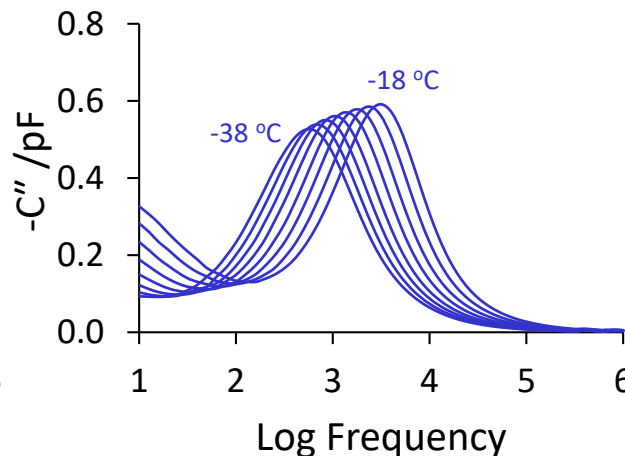
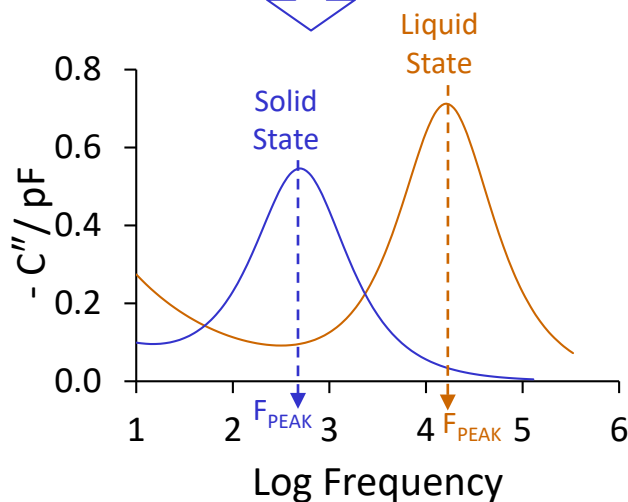
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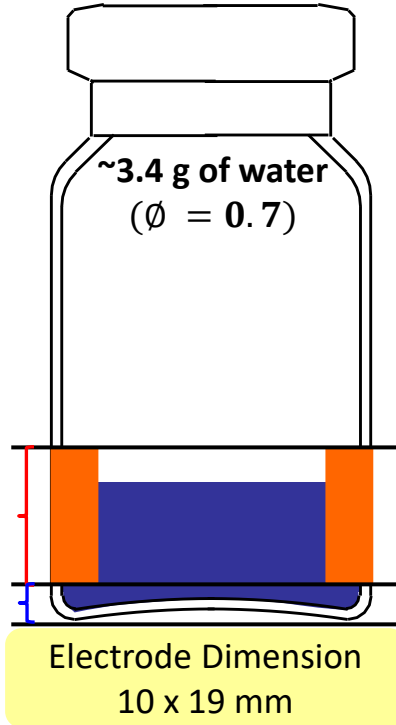
Surrogate **drying rate**  
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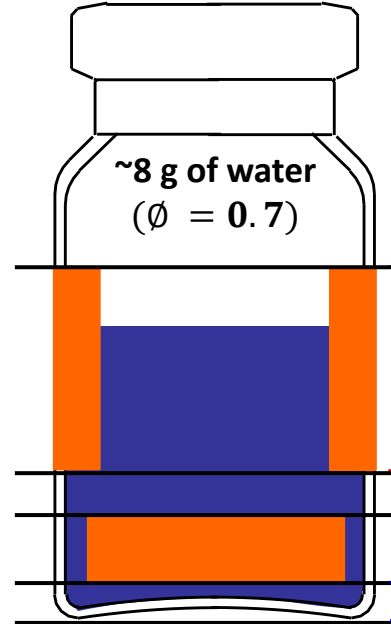
$C'$  (~ 100 kHz) is highly sensitive to low ice volumes; therefore it could be used for determination **end point** of primary drying

# Dual-electrode system

Standard TVIS vial  
(Single electrode system)



New feature of TVIS vial  
(Dual electrode system)



Electrode Dimension  
Top electrode (TE): 10 x 19 mm  
Bottom Electrode (BE): 5 x 19 mm

Electrode height ~10 mm  
Electrode distance from base  
~3 mm

Top electrode height ~15 mm

Gap between electrode ~3 mm

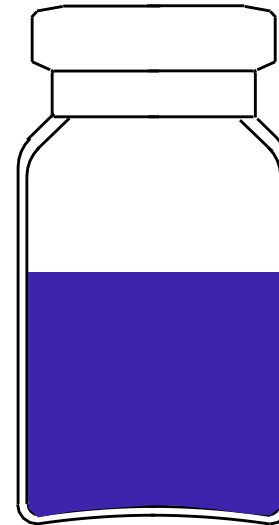
Bottom electrode height ~10 mm

Electrode distance from base  
~3 mm

- A dual electrode system comprises two pairs of copper electrode glued to the external surface of a Type I tubular glass vial.
- This option is suitable for large volume samples, including those used for  $K_v$  determination.

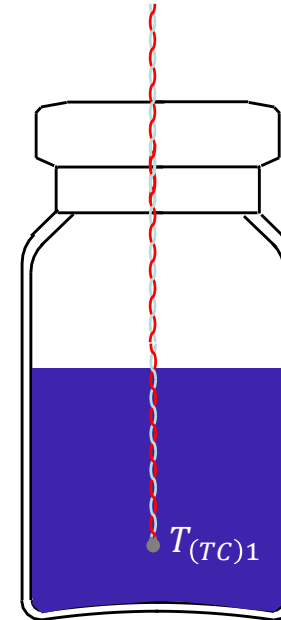
# Multiplexing PAT – Case study

- Combination of two single vial process analytics
  - Thermocouple (TC)
  - Through Vial Impedance Spectroscopy (TVIS)
- Ideal scenario :
  - Both measurements on the same vial
- Challenges with TC
  - provides additional nucleation sites (early onset ice nucleation) and a heat source (increased localised drying rate)
  - Loss of contact when positioned close to the sublimation interface (can not measure ice interface temperatures)



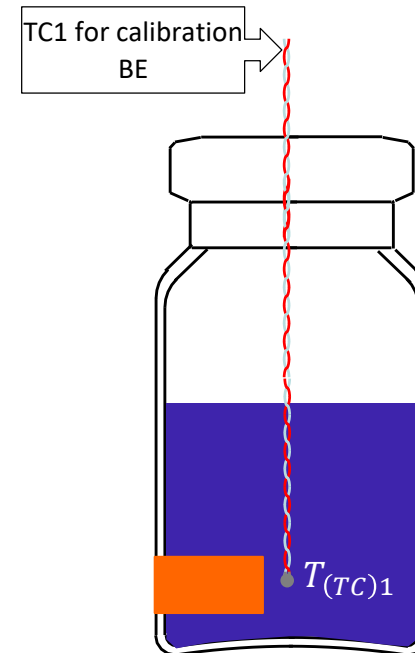
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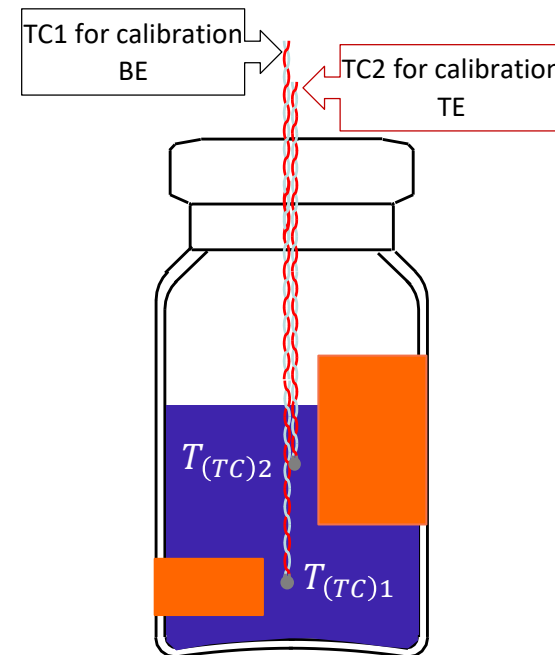
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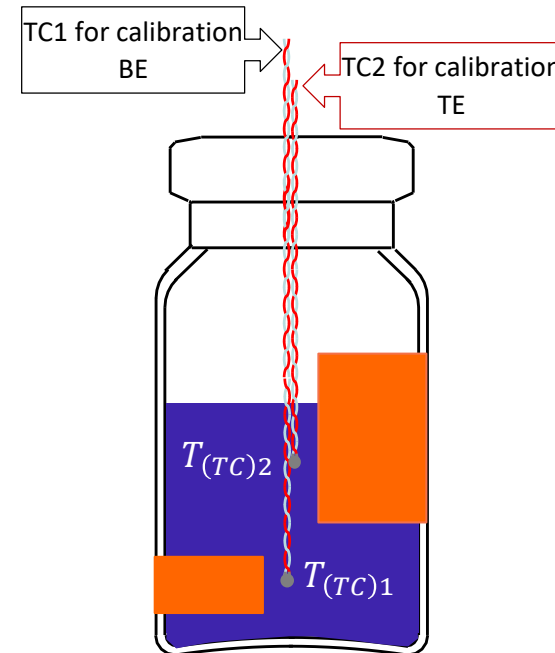
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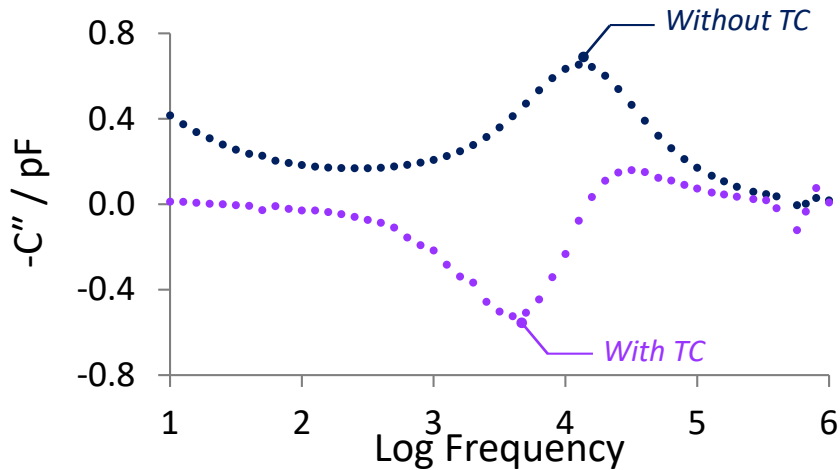
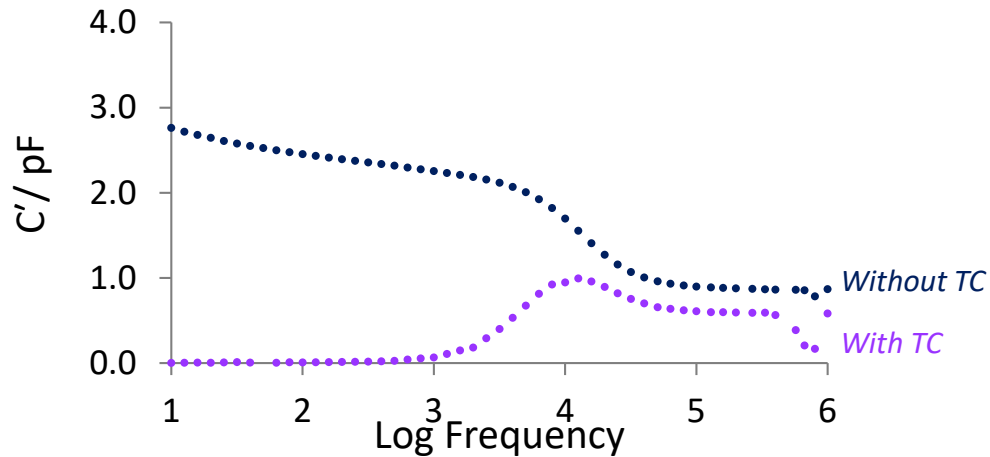
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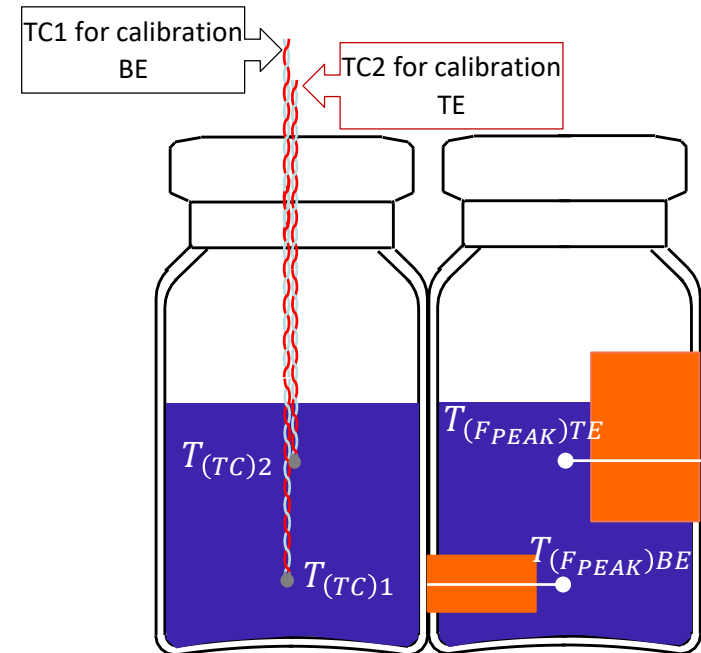


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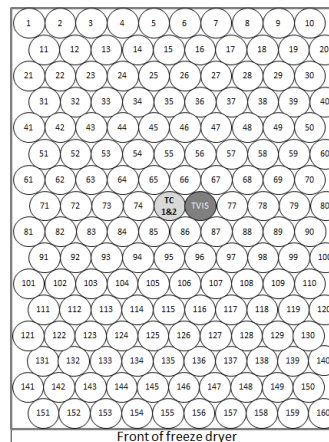
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# Through Vial Impedance Spectroscopy (TVIS)

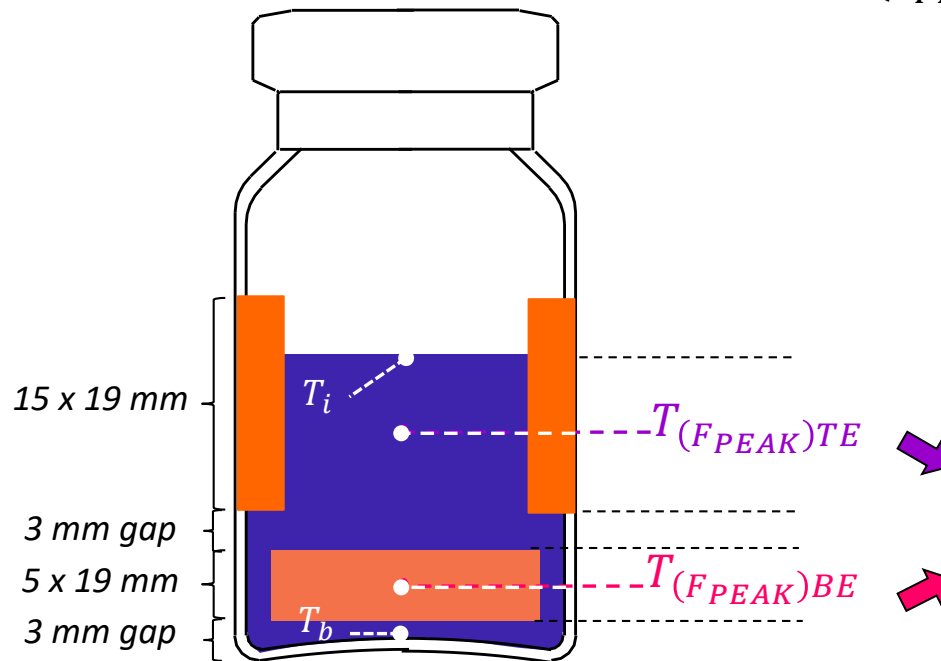
## *Dual-electrode system and its applications*

### *(Ice temperature, Drying rate and Heat transfer coefficient )*



# Temperature Determination

## Dual electrode



- $T_{(F_{PEAK})TE}$  : TVIS predicted temperature from top electrode (TE)
- $T_{(F_{PEAK})BE}$  : TVIS predicted temperature from bottom electrode (BE)

Both  $T_i$  and  $T_b$  can be estimated by extrapolating from the temperatures predicted from the centers of top electrode ( $T_{(F_{PEAK})TE}$ ) and bottom electrode ( $T_{(F_{PEAK})BE}$ ).

# Aims & Objectives

## Aims

To determine the heat transfer coefficient ( $K_v$ ) by using a novel dual electrode TVIS approach

- I Temperature calibration of  $\log F_{PEAK}$  of top electrode ( $T_{(F_{PEAK})TE}$ ) and bottom electrode ( $T_{(F_{PEAK})BE}$ )
- II Prediction ice temperatures for both electrodes during primary drying
- III Temperature calibration of  $C''_{PEAK}$
- IV Compensation of  $C''_{PEAK}$  during primary drying
- V Calibration of  $C''_{PEAK}$  for ice layer height
- VI Estimation of ice layer height during primary drying
- VII Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )
- VIII Comparison of TVIS drying rate ( $\Delta m/\Delta t$ ) with gravimetric method (weight loss)
- IX Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period
- X Heat transfer coefficient ( $K_v$ ) calculation

## Objective

I

Temperature calibration of  $\log F_{PEAK}$  of top electrode ( $T_{(F_{PEAK})TE}$ ) and bottom electrode ( $T_{(F_{PEAK})BE}$ )

Annealing the sample

In-line TVIS measurement

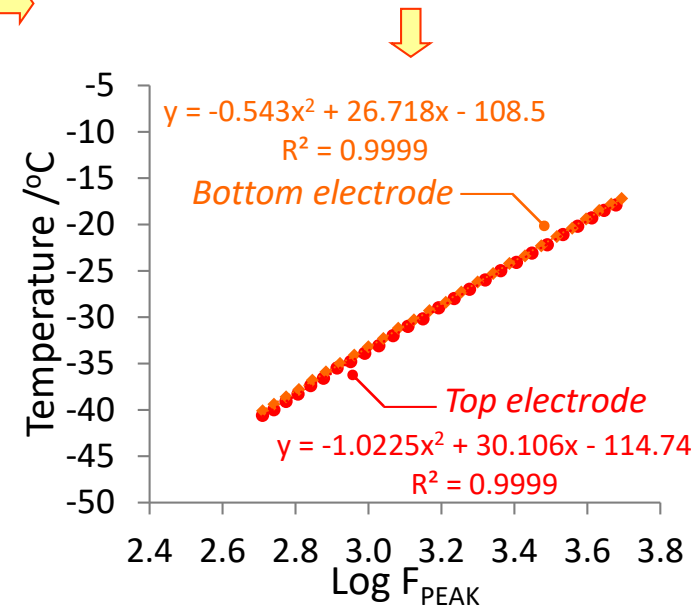
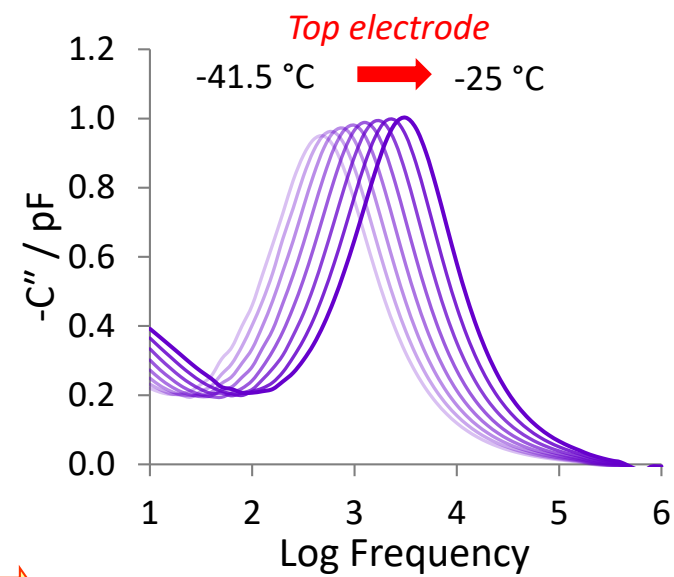
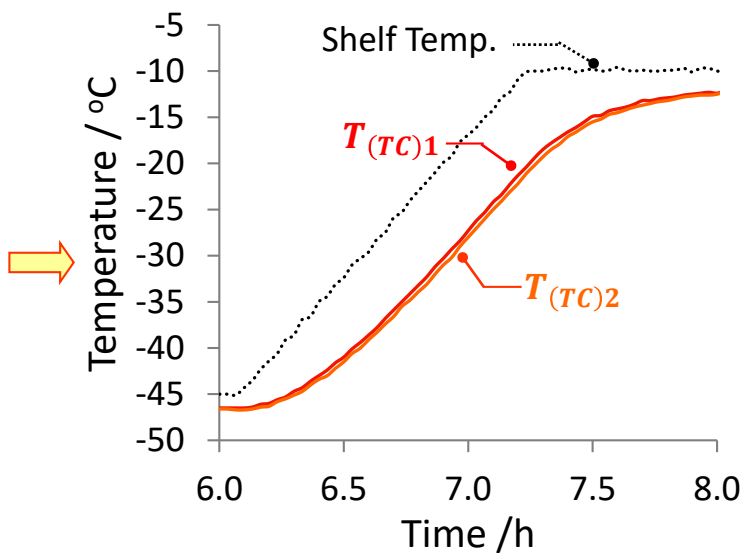
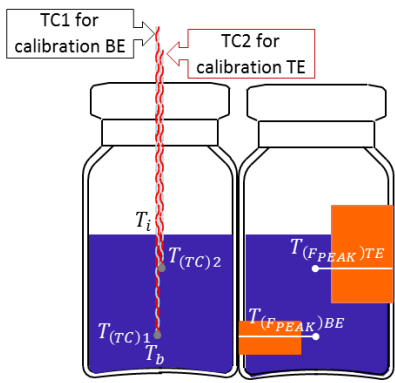
Identifying peak frequency ( $F_{PEAK}$ ) using LyoView™ software

Calibration plot (temperature vs  $\log F_{PEAK}$ )

Predicting product temperature using calibration plot

# Objective

I Temperature calibration of  $\log F_{PEAK}$  of top electrode ( $T_{(F_{PEAK})TE}$ ) and bottom electrode ( $T_{(F_{PEAK})BE}$ )



Polynomial coefficient from  $\log F_{PEAK}$  – temperature calibration

|    | $a$                    | $b$  | $c$  |
|----|------------------------|------|------|
| TE | -1.02                  | 30.1 | -114 |
| BE | $-5.43 \times 10^{-1}$ | 26.7 | -109 |

## Objective

II

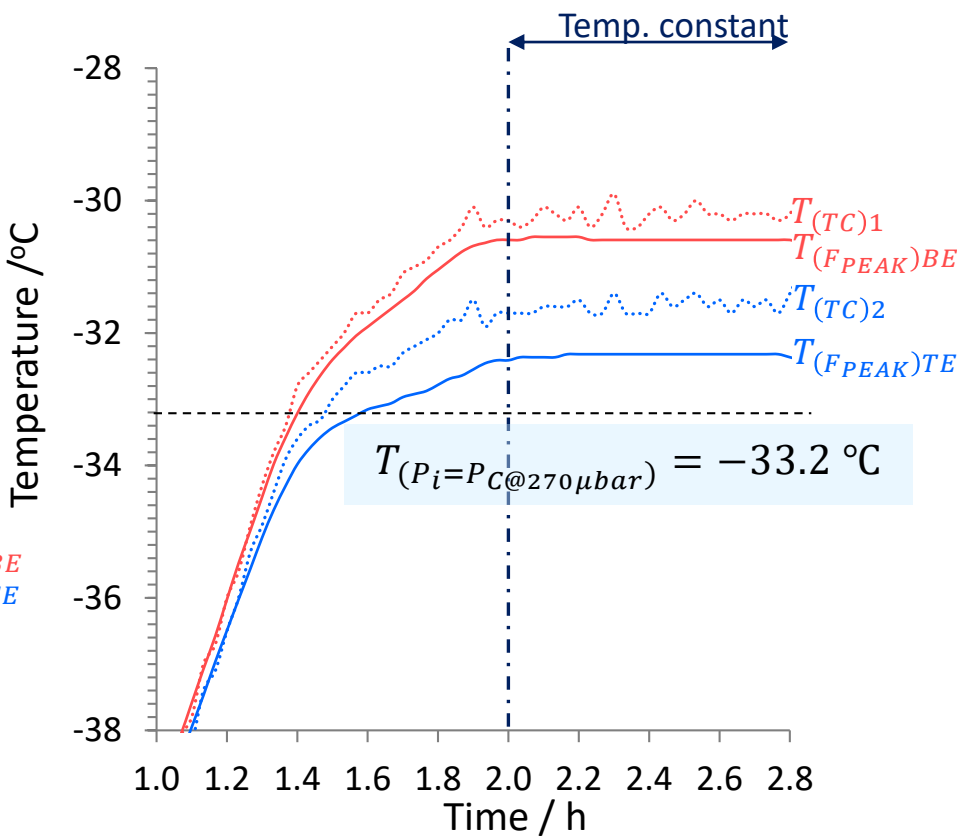
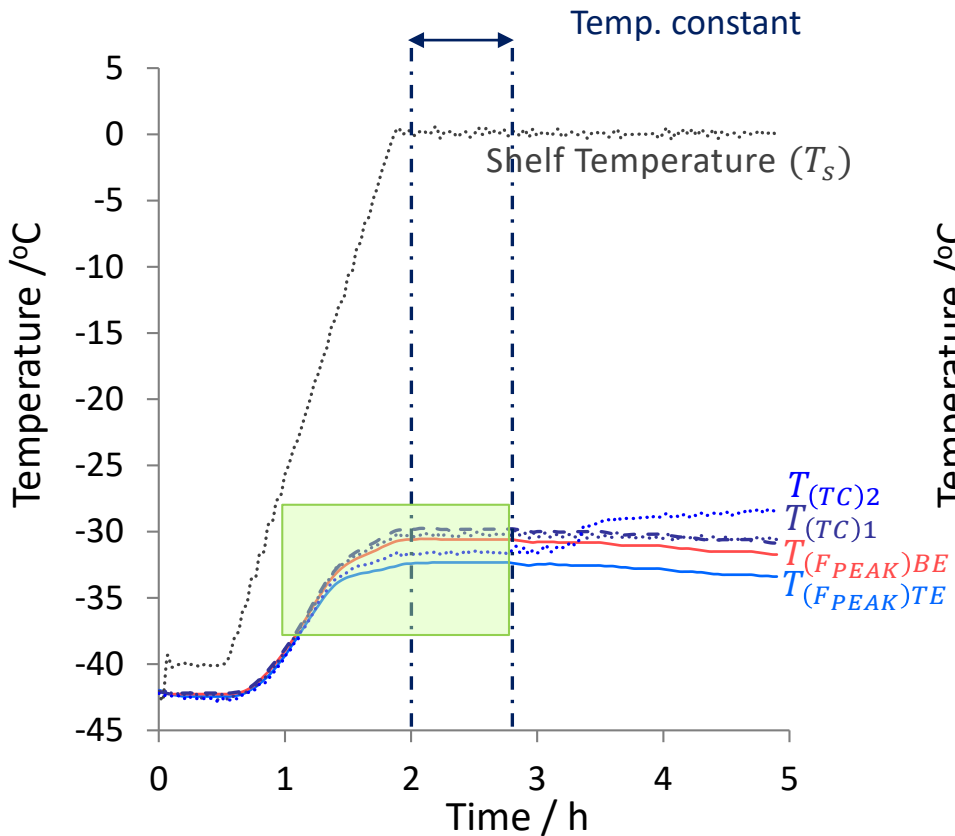
Prediction ice temperatures for both electrodes during primary drying



# Objective

II

Prediction ice temperatures for both electrodes during primary drying



The product temperature predicted by TVIS can demonstrate the temperature gradient across ice cylinder height

## Objective

### III

Temperature calibration of  $C''_{PEAK}$

Annealing the sample

In-line TVIS measurement

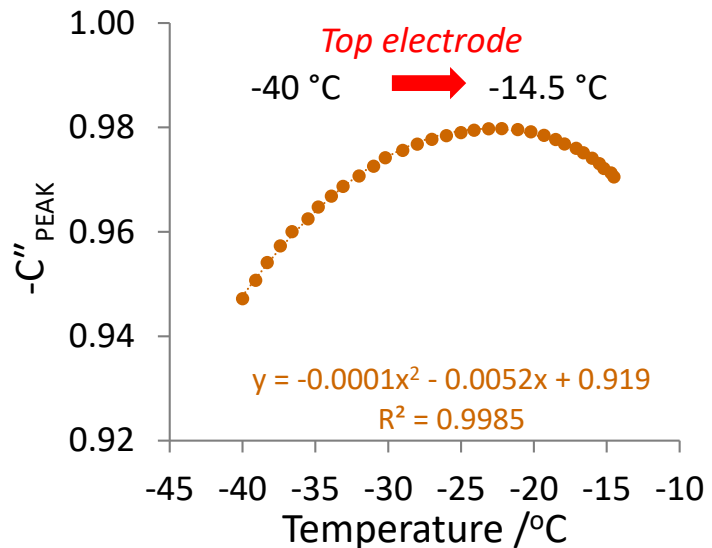
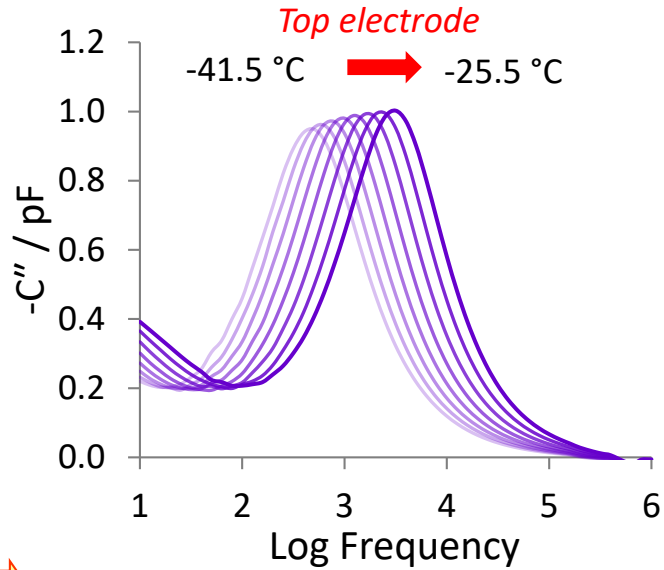
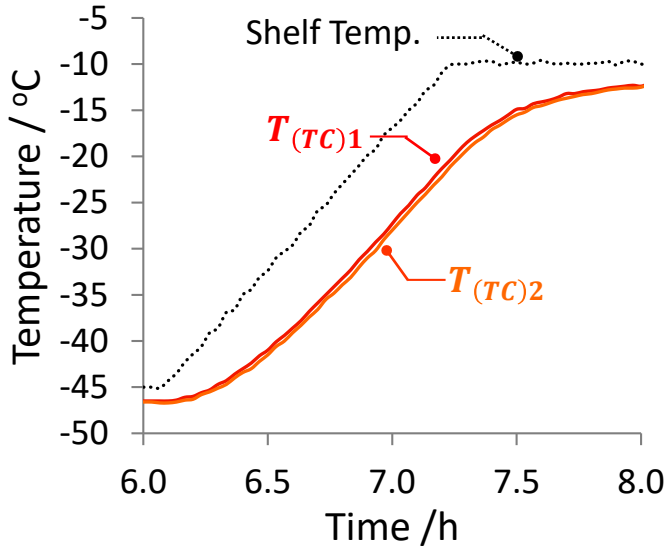
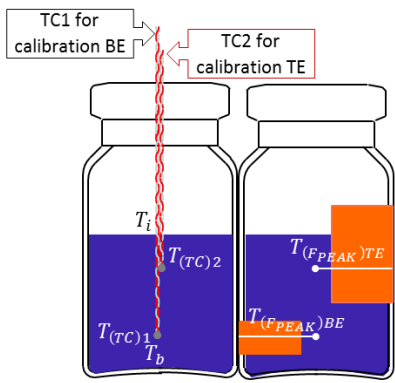
Identifying peak amplitude ( $C''_{PEAK}$ ) using LyoView™ software

Calibration plot ( $C''_{PEAK}$  vs temperature)

Temperature compensation of  $C''_{PEAK}$  using calibration plot

# Objective

## III Temperature calibration of $C''_{PEAK}$



Polynomial coefficient from  $C''_{PEAK}$  – temperature calibration

| $a$                    | $b$                    | $c$                   |
|------------------------|------------------------|-----------------------|
| $-1.00 \times 10^{-4}$ | $-5.20 \times 10^{-3}$ | $9.19 \times 10^{-1}$ |

## Objective

IV

Compensation of  $C''_{PEAK}$  during primary drying

## Objective

## IV

Compensation of  $C''_{PEAK}$  during primary drying

- During primary drying,  $C''_{PEAK}$  is attributed to both the loss of ice and product temperature; therefore, it requires a standardization factor ( $\emptyset$ ) for temperature compensation:

$$\emptyset(T) = \frac{C''_{PEAK}(T)}{C''_{PEAK}(T_{ref})}$$

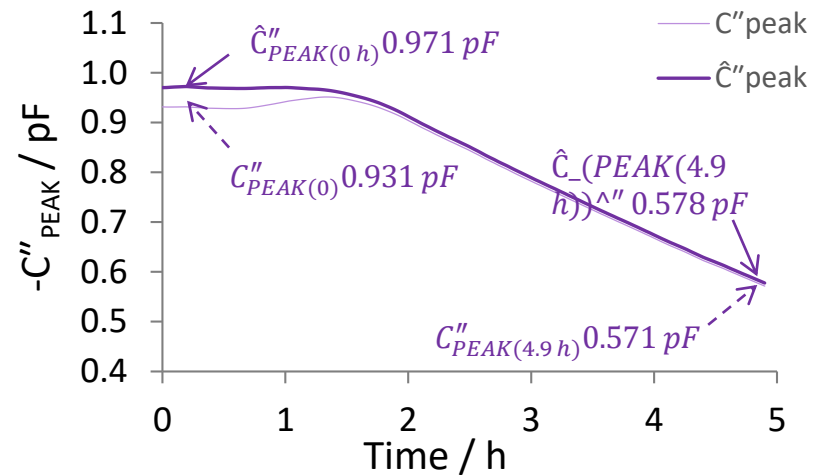
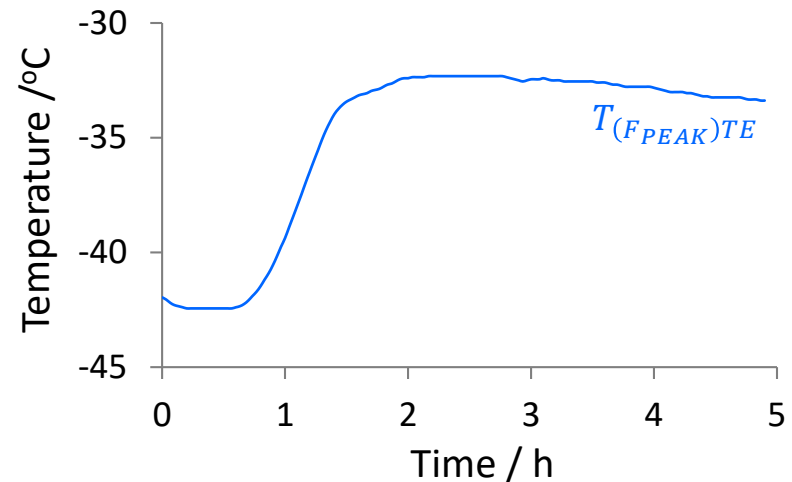
$C''_{PEAK}(T)$  and  $C''_{PEAK}(T_{ref})$  are the peak amplitudes at temperatures ( $T$ ) and reference temperature ( $T_{ref}$ ) during the re-heating ramp. In this presentation, a temperature of  $-20^\circ\text{C}$  is used as the reference temperature value

- The expression for  $\emptyset(T)$  can be re-written in terms of the polynomial coefficients (slide 22):

$$\emptyset(T) = \frac{aT^2 + bT + c}{aT_{ref}^2 + bT_{ref} + c}$$

- Values of  $C''_{PEAK}$  during primary drying are then standardized to the reference temperature by dividing by  $\emptyset(T)$  to give a standardized peak amplitude of  $\hat{C}''_{PEAK}$

$$\hat{C}''_{PEAK} = \frac{C''_{PEAK}(T)}{\emptyset(T)}$$



The standardized  $C''_{PEAK}$  is defined as  $\hat{C}''_{PEAK}$

## Objective

V

Calibration of  $C''_{PEAK}$  for ice layer height

Filling water  
into TVIS vial

Freezing the  
sample

In-line TVIS  
measurement

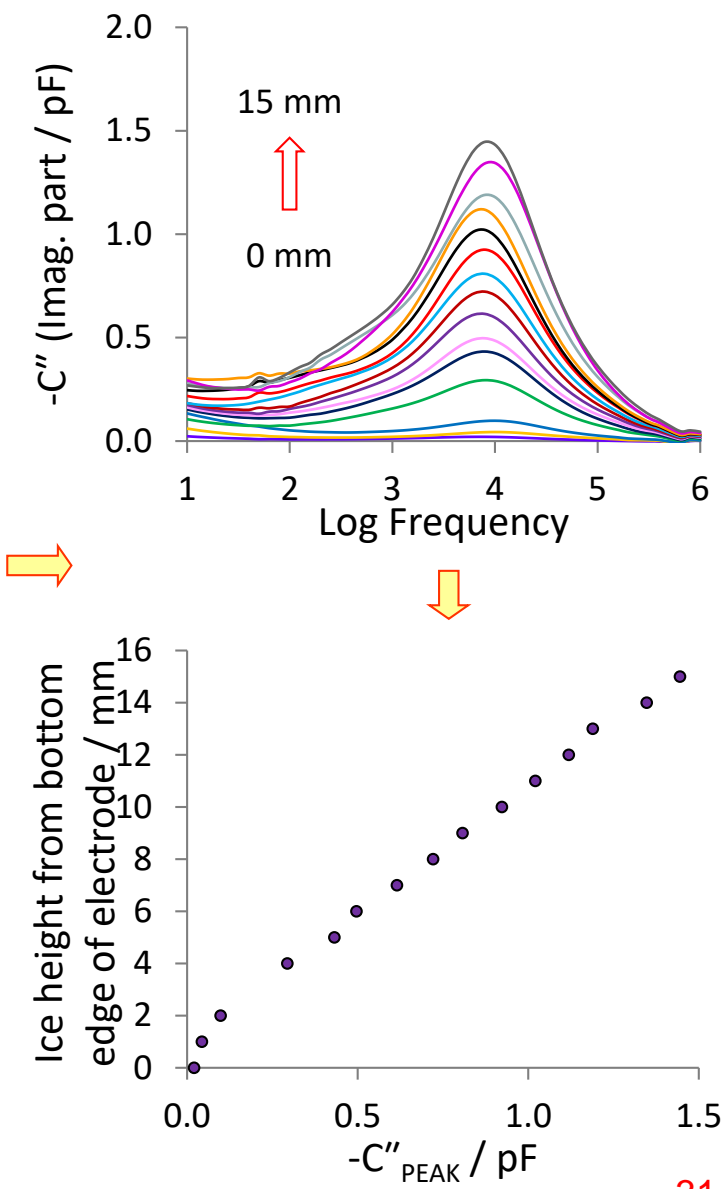
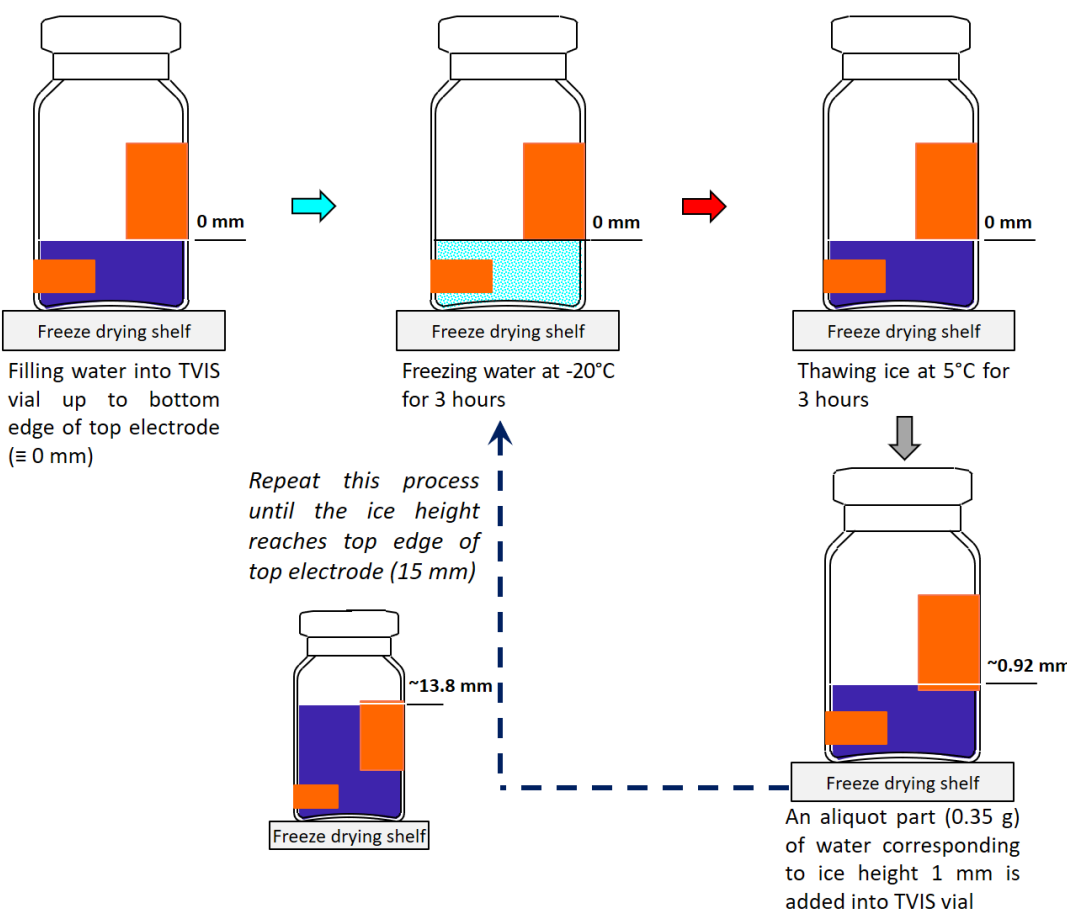
Thawing the  
sample

Identifying  
 $C''_{PEAK}$  using  
simple peak  
finding

Calibration plot  
( $C''_{PEAK}$  vs  
temperature)

# Objective

V Calibration of  $C''_{PEAK}$  for ice layer height



## Objective

VI

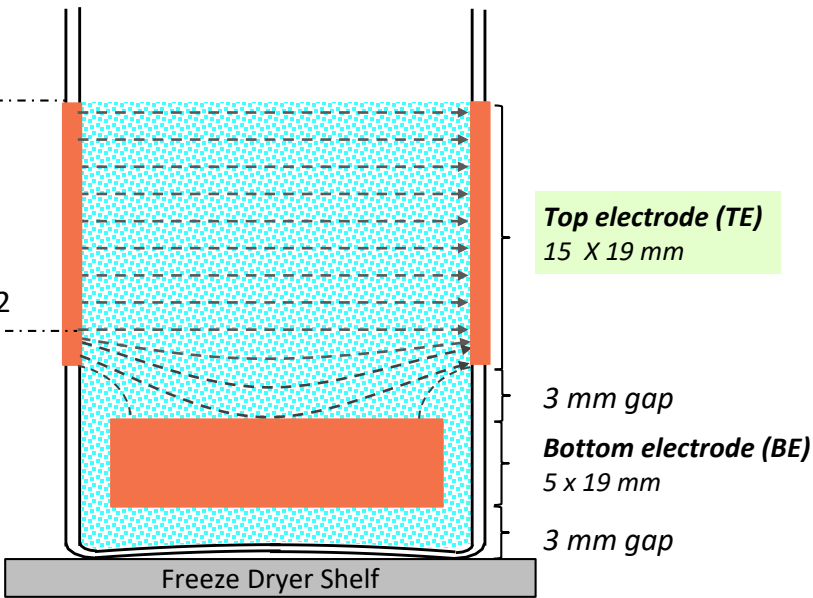
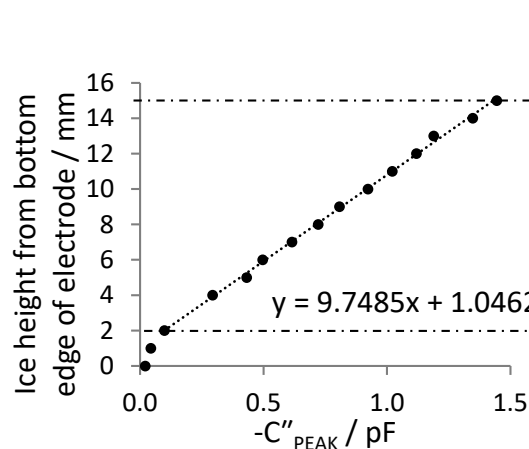
Estimation of ice layer height during primary drying



VI Estimation of ice layer height during primary drying



At -20 °C



$$\text{Ice height}(h) = 9.7485 \times C''_{PEAK} + 1.0462$$

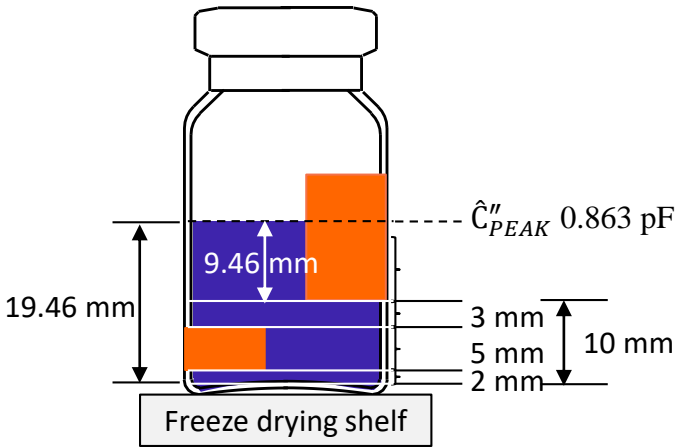
Gradient of the line ( $m_{h/c}$ )

At 2.4 h into primary drying

$\hat{C}''_{PEAK} = 0.863 \text{ pF}$

Ice height =  $9.7485 \times 0.863 + 1.0462$   
= 9.459 mm (from the bottom edge of TE)

Ice front height =  $9.459 + (2 + 5 + 3)$   
= **19.46 mm**

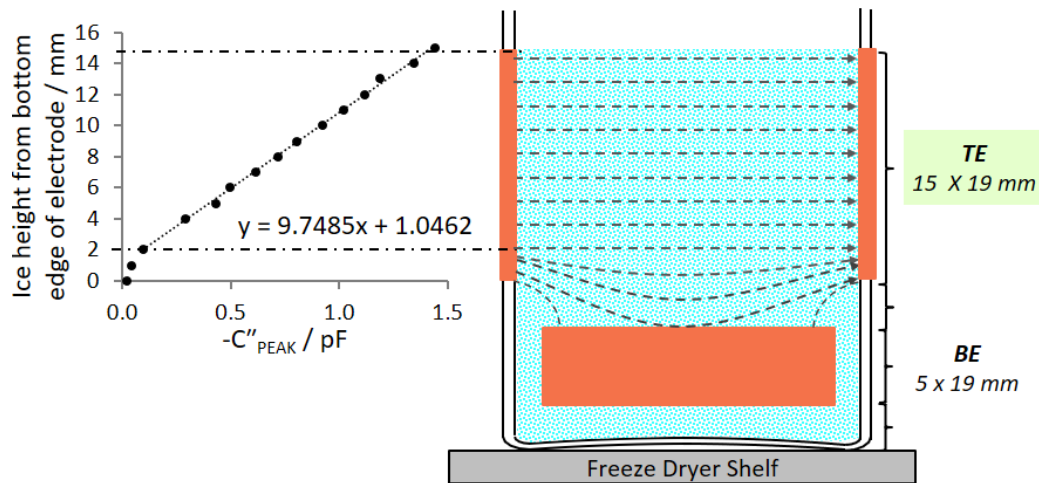


## Objective

## VI

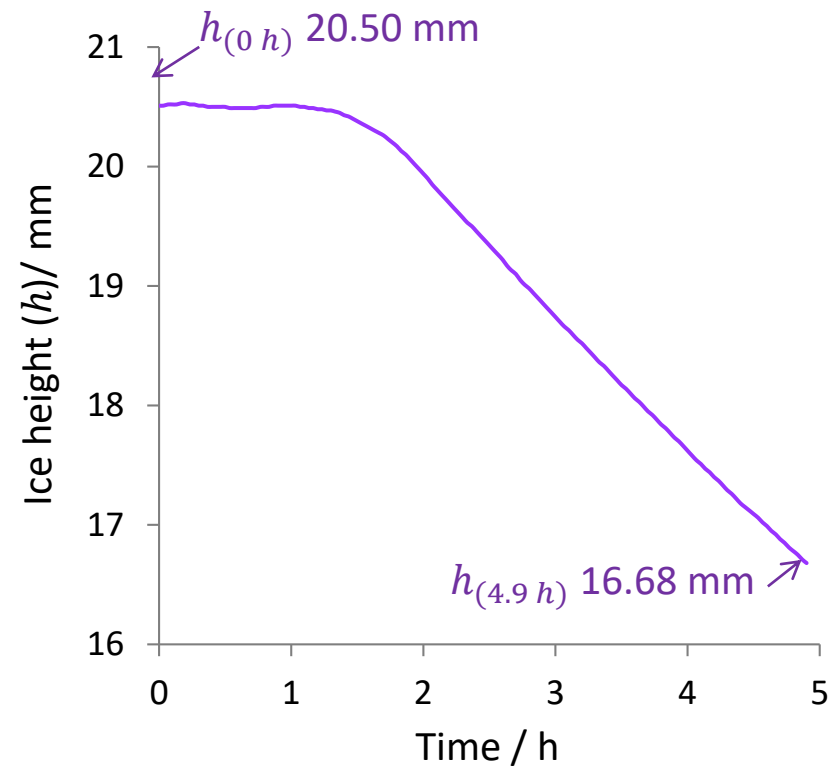
## Estimation of ice layer height during primary drying

- The dependency of  $C''_{PEAK}$  on the ice cylinder height in linear region
- Surrogate drying rate can be estimated in terms of decreasing ice height



$$y = 9.7485x + 1.0462$$

$\downarrow$  Linear gradient ( $m_{h/c}$ )  
 $\downarrow$  Ice height ( $h$ )  
 $\downarrow$   $C''_{PEAK}$



## Objective

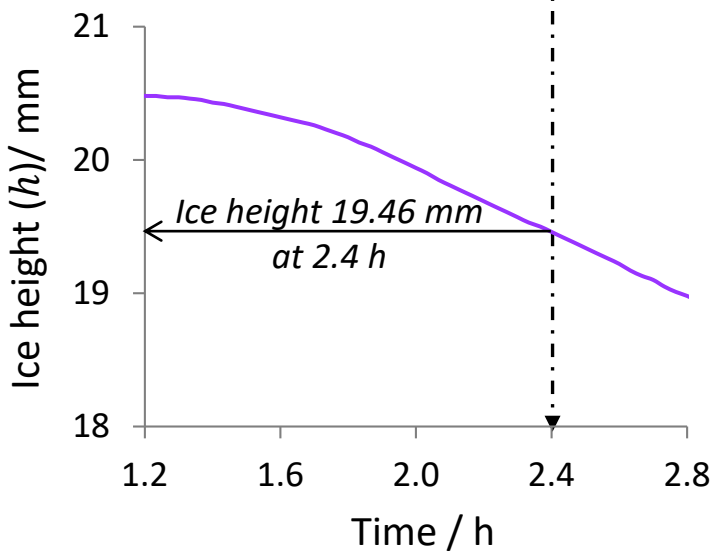
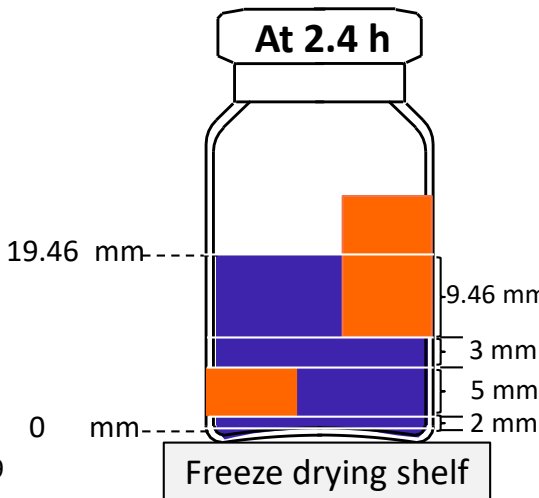
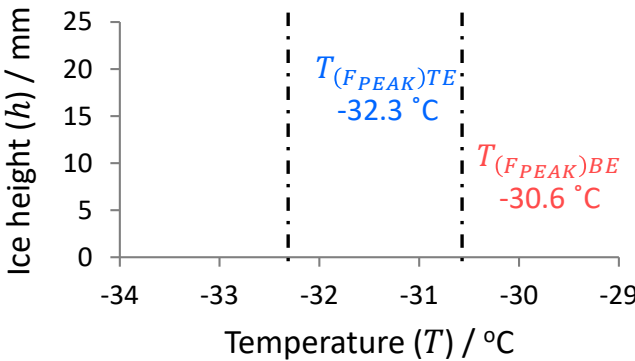
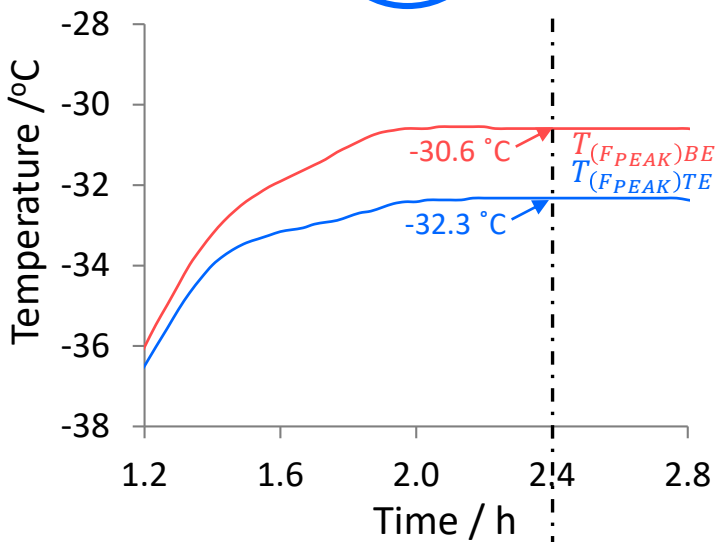
VII

Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )

# Objective

## VII

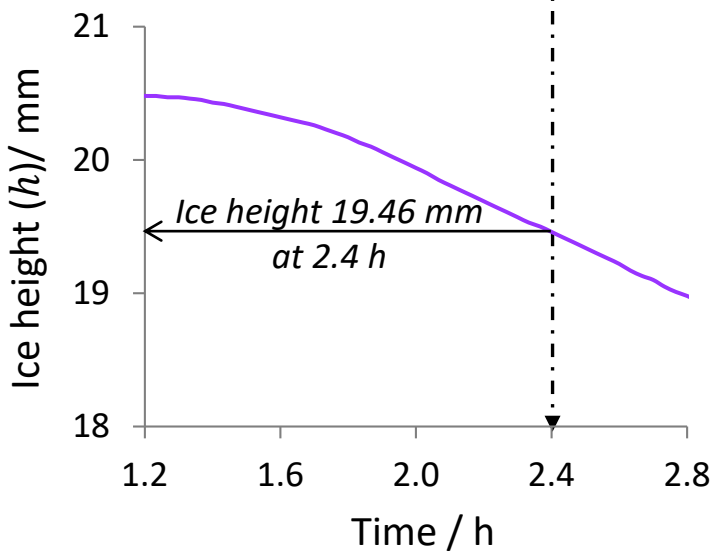
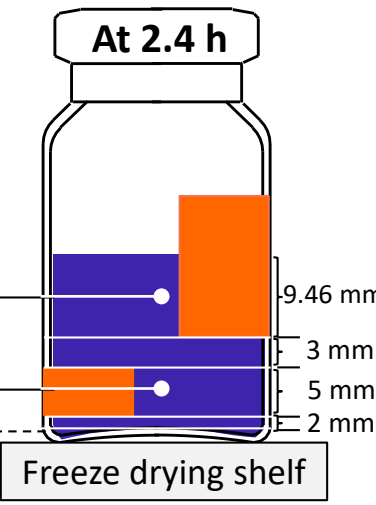
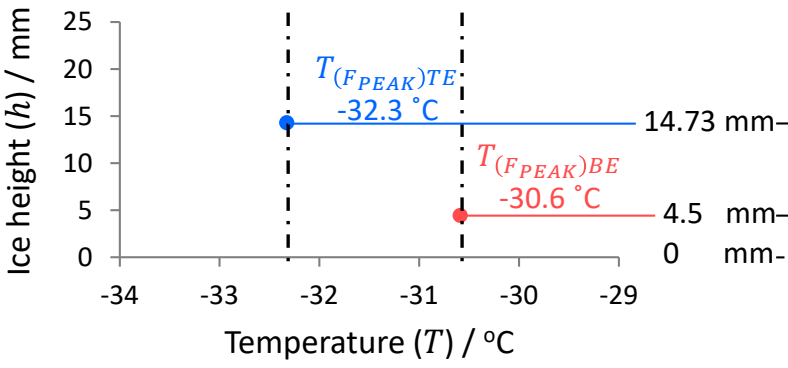
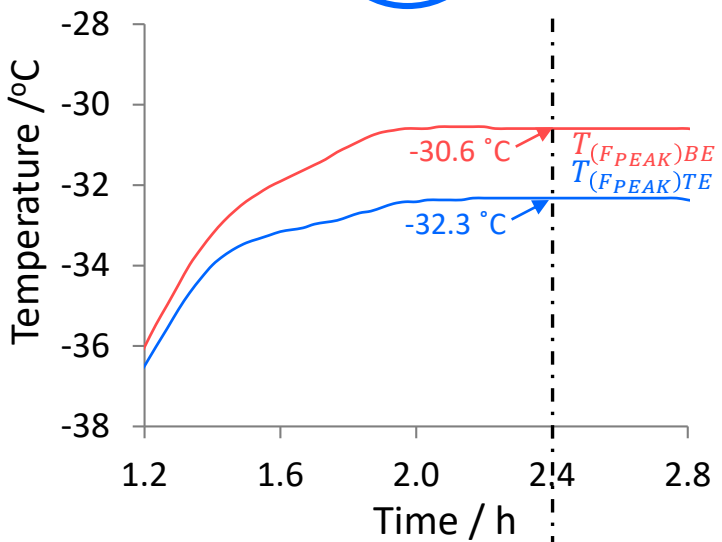
Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )



# Objective

## VII

Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )



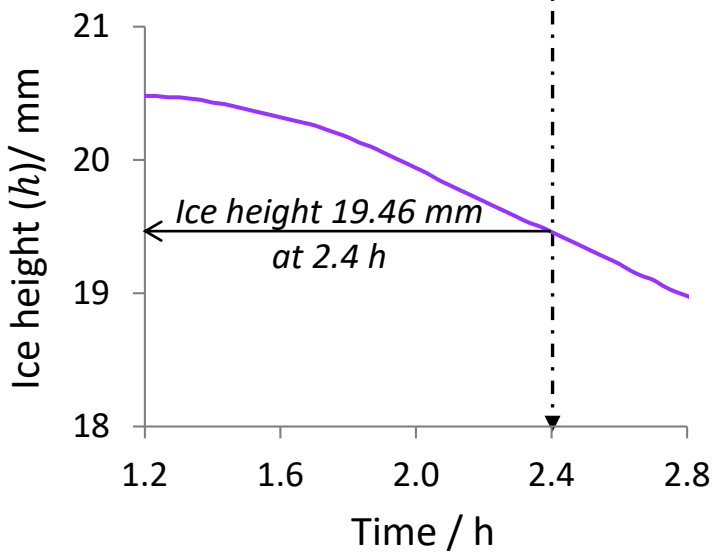
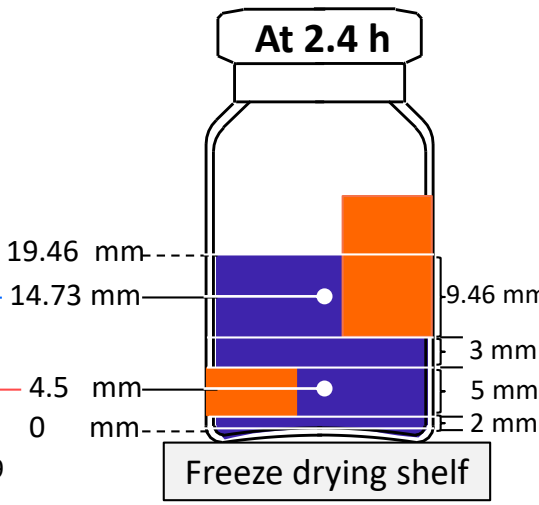
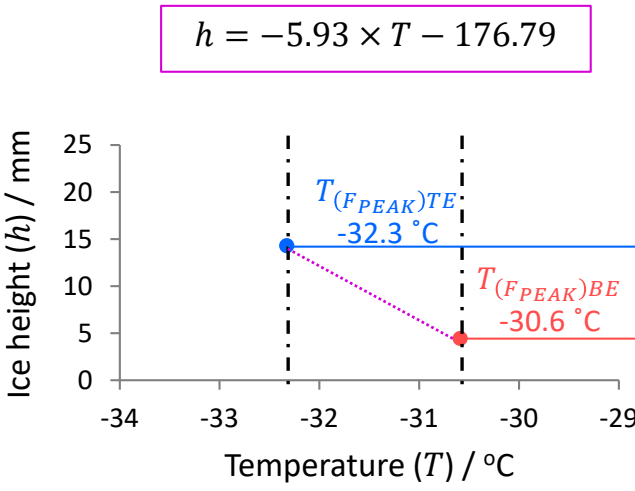
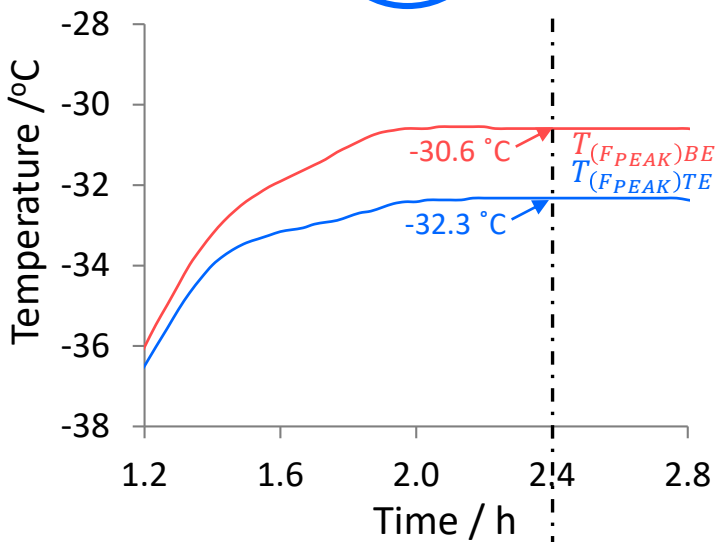
Ice height for  $T_{(FPEAK)TE}$  =  $2 + 5 + 3 + (\frac{9.46}{2}) = 14.73 \text{ mm}$

Ice height for  $T_{(FPEAK)BE}$  =  $2 + (\frac{5}{2}) = 4.50 \text{ mm}$

# Objective

## VII

Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )



Ice height for  $T_{(FPEAK)TE}$  =  $2 + 5 + 3 + (\frac{9.46}{2}) = 14.73$  mm

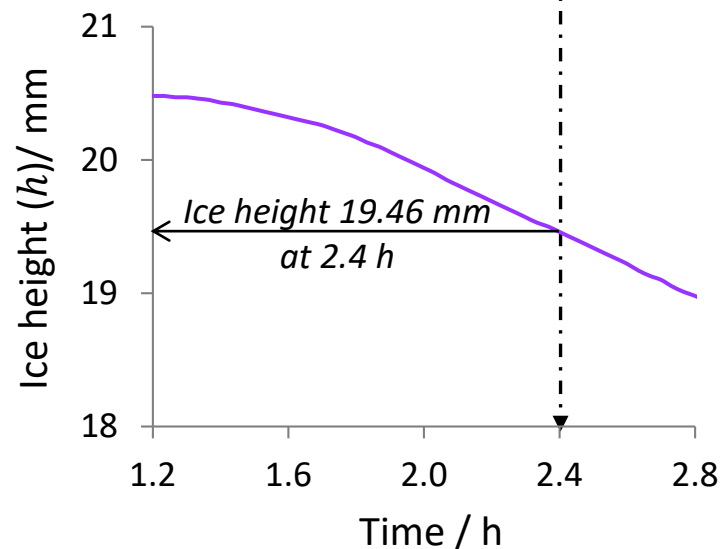
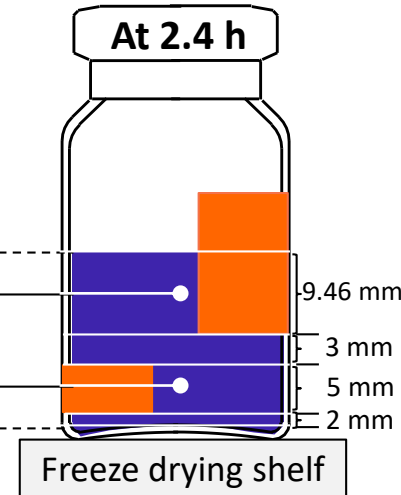
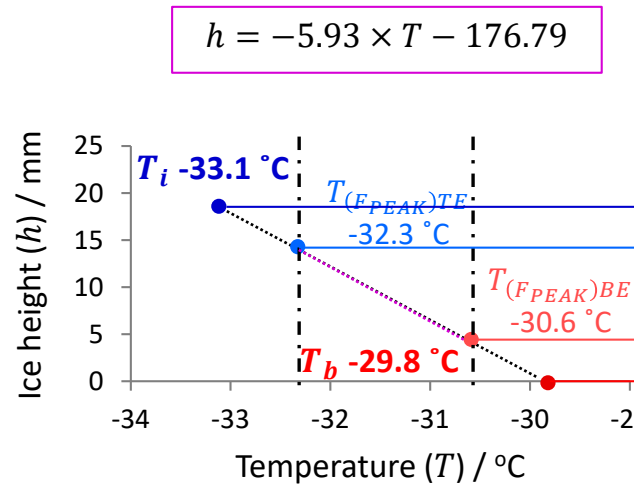
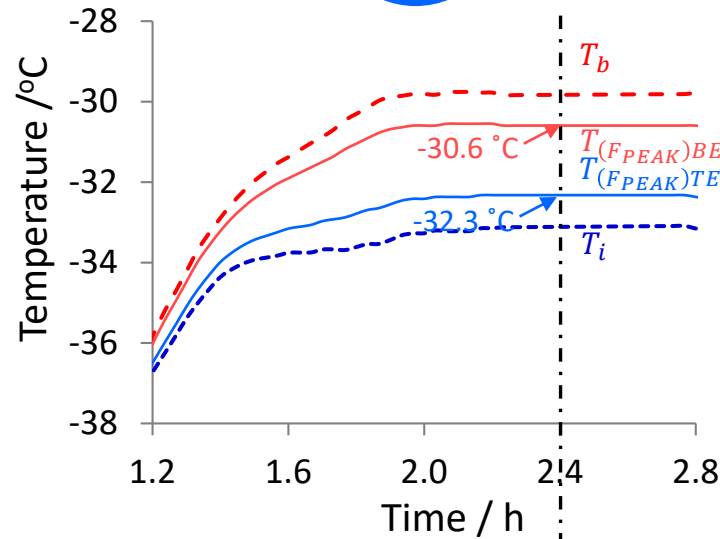
Ice height for  $T_{(FPEAK)BE}$  =  $2 + (\frac{5}{2}) = 4.50$  mm

$h = -5.93 \times T - 176.79$   $\Rightarrow$   $T = \frac{h + 176.79}{-5.93}$

# Objective

VII

Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_c)}$ )



$$\text{Ice height for } T_{(FPEAK)TE} = 2 + 5 + 3 + \left(\frac{9.46}{2}\right) = 14.73 \text{ mm}$$

$$\text{Ice height for } T_{(FPEAK)BE} = 2 + \left(\frac{5}{2}\right) = 4.50 \text{ mm}$$

$$h = -5.93 \times T - 176.79$$



$$T = \frac{h + 176.79}{-5.93}$$

## Ice Temperature

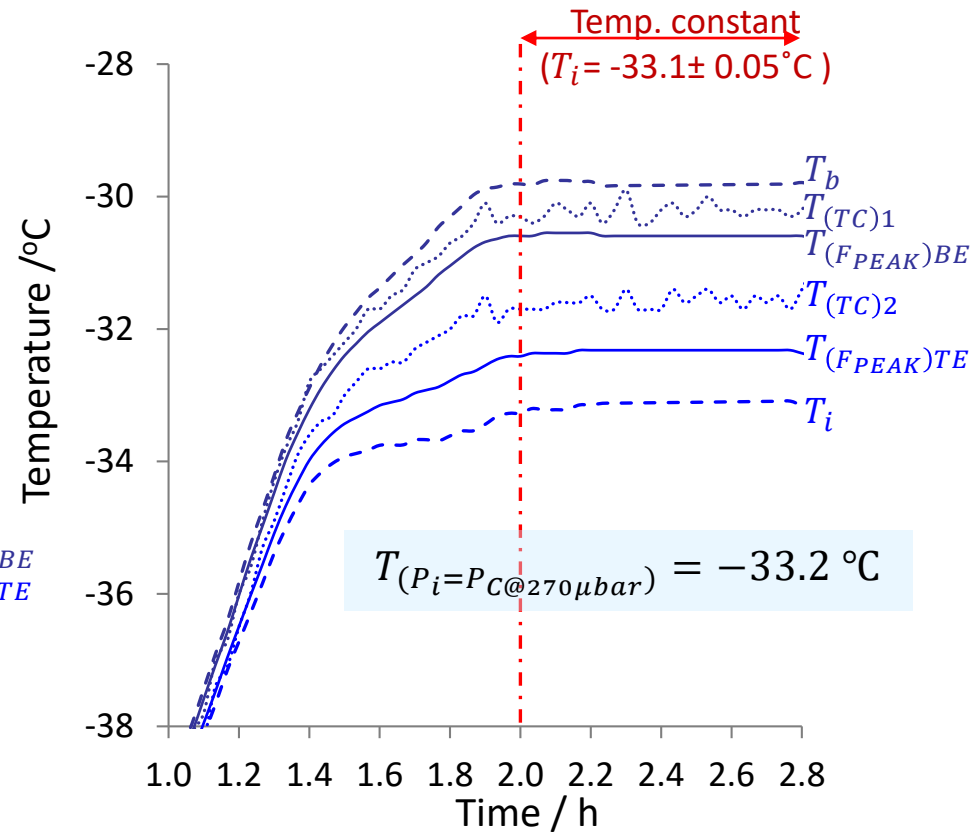
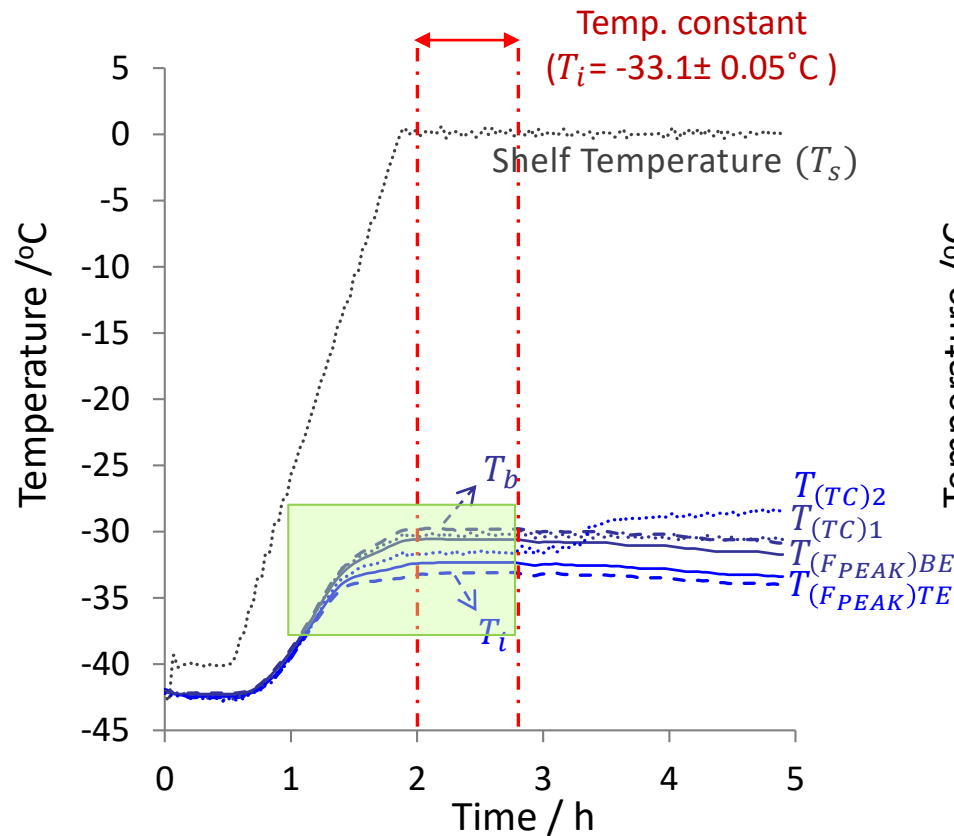
$$\text{At interface } (T_i, 19.46 \text{ mm}) = \frac{h + 176.79}{-5.93} = \frac{19.46 + 176.79}{-5.93} = -33.1 \text{ }^{\circ}\text{C}$$

$$\text{At vial's base } (T_b, 0 \text{ mm}) = \frac{h + 176.79}{-5.93} = \frac{0 + 176.79}{-5.93} = -29.8 \text{ }^{\circ}\text{C}$$

## Objective

VII

Prediction ice temperatures at (i) sublimation interface ( $T_i$ ) and (ii) vial's base ( $T_b$ ) including qualification TVIS technique ( $T_i = T_{(P_i=P_C)}$ )



The product temperature at ice interface predicted by using a 2-points temperature extrapolation close to the temperature of ice vapour at chamber pressure of 270  $\mu\text{bar}$  ( $T_{(P_i=P_C@270\mu\text{bar})}$ )



## Objective

VIII

Comparison of TVIS drying rate (  $\Delta m / \Delta t$  ) with gravimetric method (weight loss)

- Drying rate calculation is based on a cylinder of ice that is reducing in height ( $h$ ) but has a constant sublimation area ( $A$ )
- The change in ice cylinder height ( $h$ ) can be equated to the change in ice volume ( $v$ )  
$$v \text{ (cylinder)} = \pi r^2 h = Ah$$

Where  $r$  is internal radius of vial and  $A$  is internal cross section area of vial ( $= \pi r^2$ )

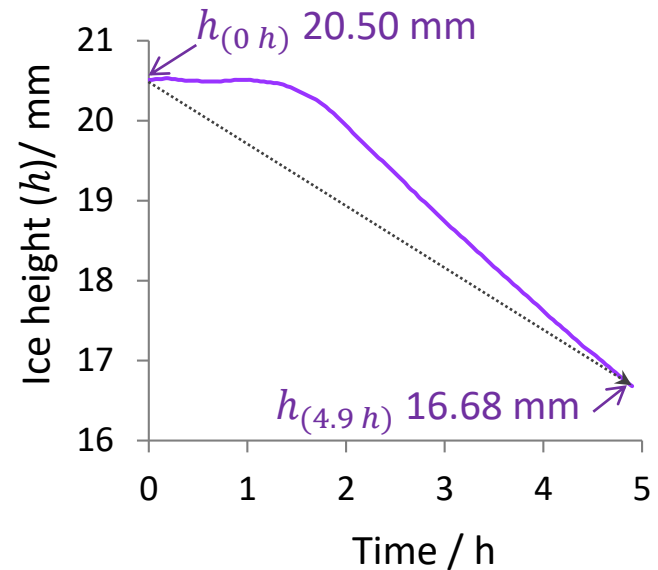
- Ice volume can be converted to ice mass ( $m$ ) by multiplying with ice density ( $\rho_i$ )  
$$m = \rho_i \cdot \pi r^2 h = \rho_i \cdot Ah$$
- Hence; drying rate ( $\frac{\Delta m}{\Delta t}$ ) can be expressed by

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t1)} - h_{(t2)}}{t_2 - t_1}$$

- An average surrogate drying rate calculation

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

|  |                            |
|--|----------------------------|
| Ice density ( $\rho_i$ ) at -32 °C     | = 0.920 g·cm <sup>-3</sup> |
| Internal vial diameter (VC010-20C)     | = 2.21 cm                  |
| Cross-section area (A)                 | = 3.80 cm <sup>2</sup>     |
| Ice height at 0 h ( $h_{(0\ h)}$ )     | = 20.50 mm                 |
| Ice height at 4.9 h ( $h_{(4.9\ h)}$ ) | = 16.68 mm                 |



$$\begin{aligned} \text{Drying rate} &= 0.920 \text{ g} \cdot \text{cm}^{-3} \times 3.80 \text{ cm}^2 \times \frac{(20.50 - 16.68) \times 10^{-1} \text{ cm}}{(4.9 - 0) \text{ h}} \\ &= 0.27 \text{ g} \cdot \text{h}^{-1} \end{aligned}$$

|             | Drying rate |
|-------------|-------------|
| TVIS        | 0.27 g/h    |
| Gravimetric | 0.25 g/h    |

## Objective

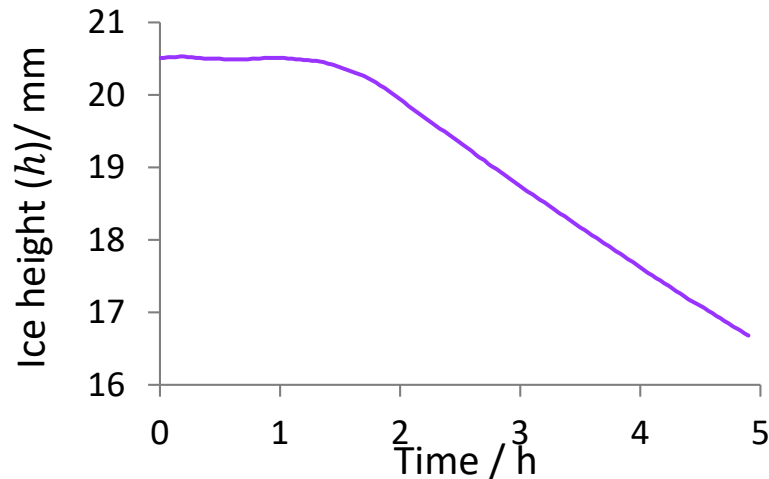
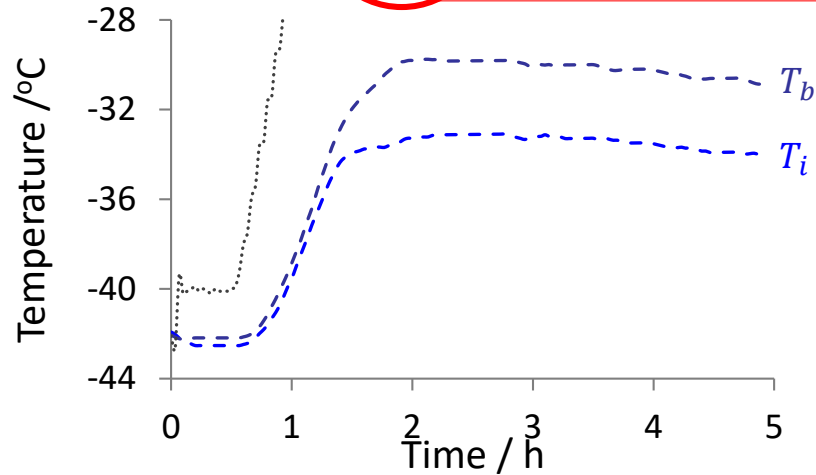
IX

Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period

# Objective

**IX**

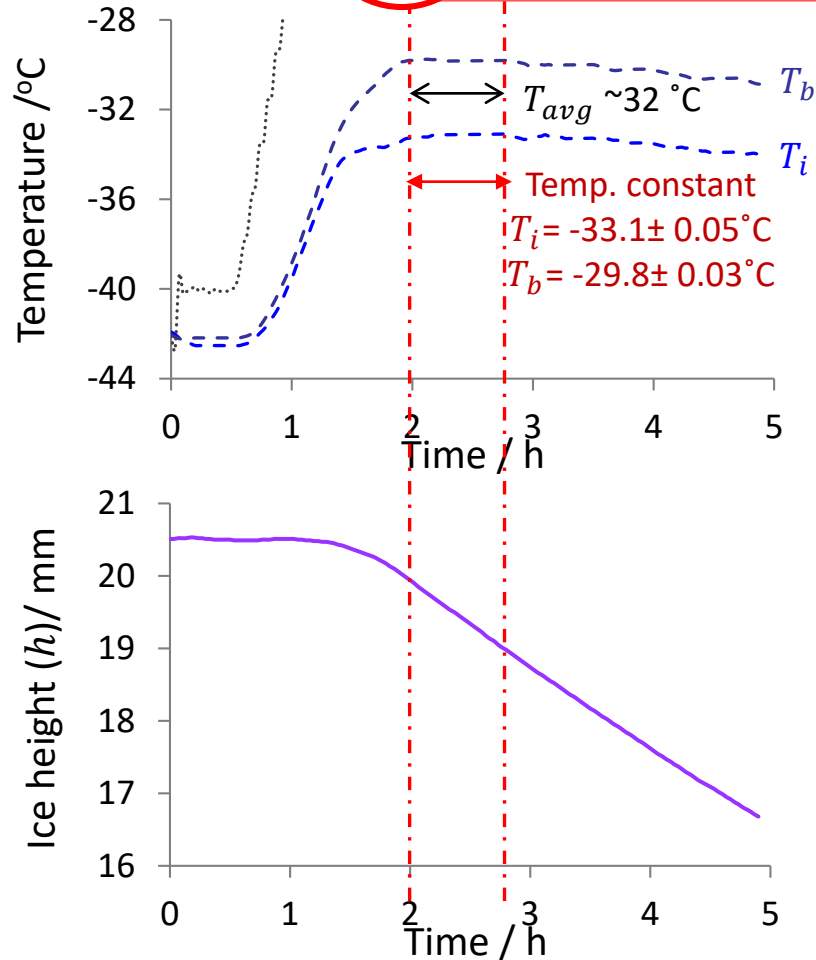
Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



# Objective

IX

Determination (i) the drying rate ( $\Delta m / \Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



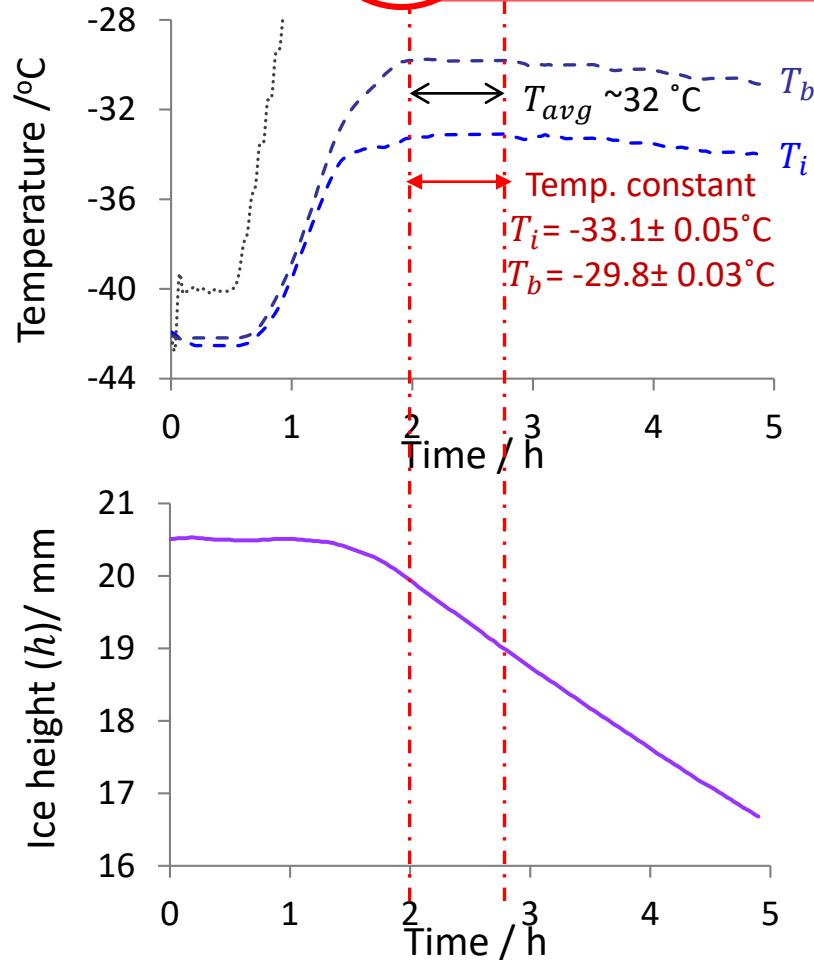
- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

# Objective

## IX

Determination (i) the drying rate ( $\Delta m / \Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

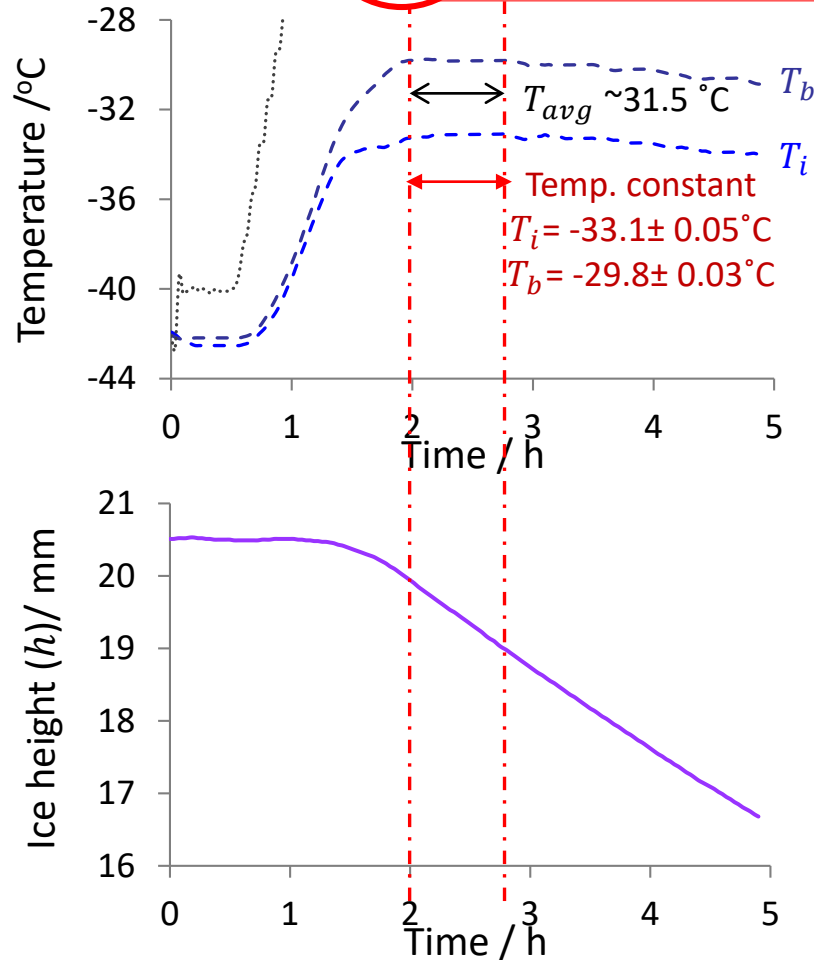
$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920 \text{ g} \cdot \text{cm}^{-3}$   
 (Calculated ice temperature between  $T_i$  &  $T_b$ )

# Objective

## IX

Determination (i) the drying rate ( $\Delta m / \Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t1)} - h_{(t2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920 \text{ g}\cdot\text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

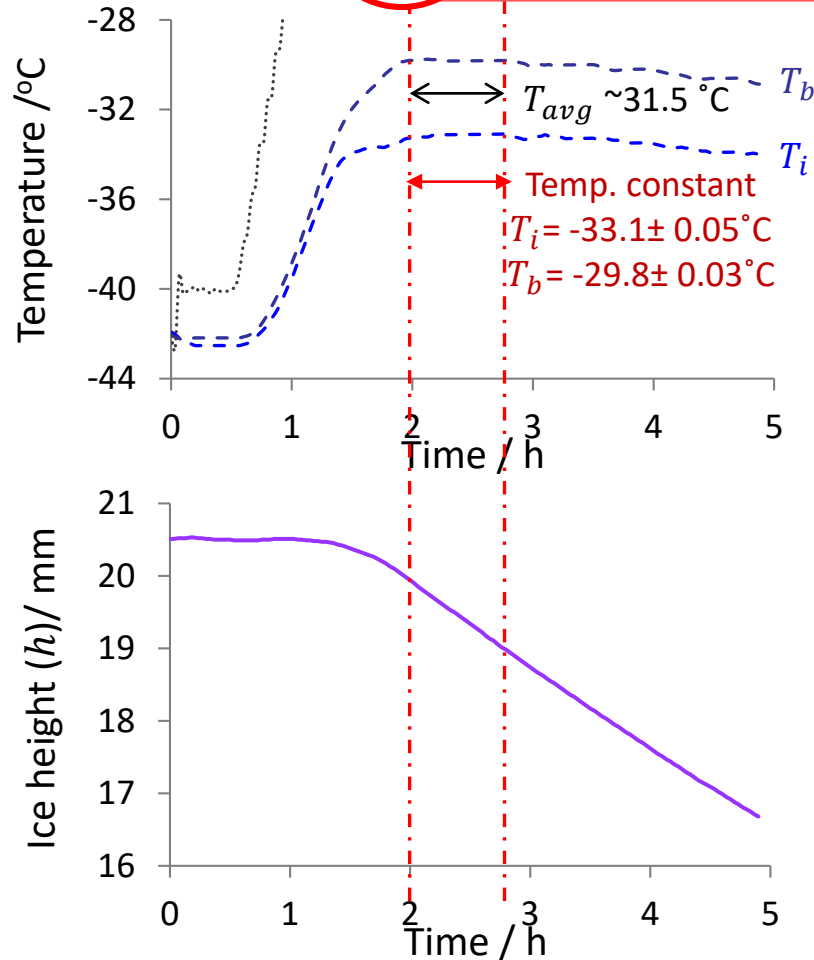
Internal vial diameter (VC010-20C) = 2.21 cm



# Objective

## IX

Determination (i) the drying rate ( $\Delta m / \Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t1)} - h_{(t2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920 \text{ g} \cdot \text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

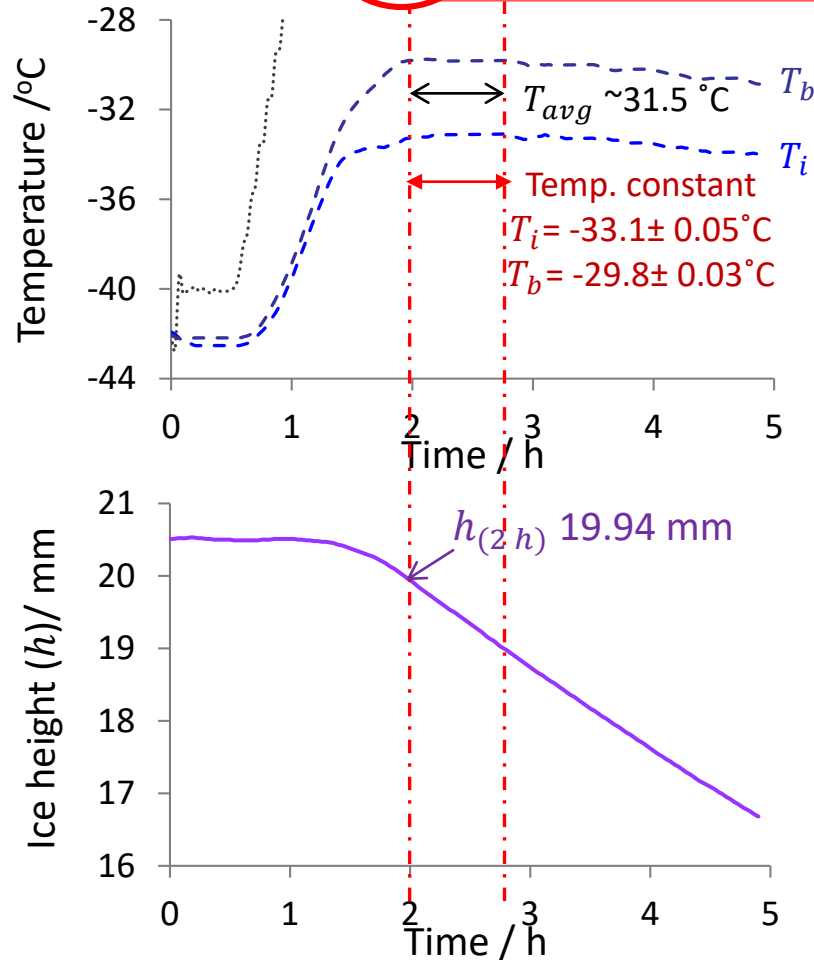
Internal vial diameter (VC010-20C) = 2.21 cm

Cross-section area ( $A$ ) =  $3.80 \text{ cm}^2$

# Objective

## IX

Determination (i) the drying rate ( $\Delta m / \Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920 \text{ g} \cdot \text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

Internal vial diameter (VC010-20C) =  $2.21 \text{ cm}$

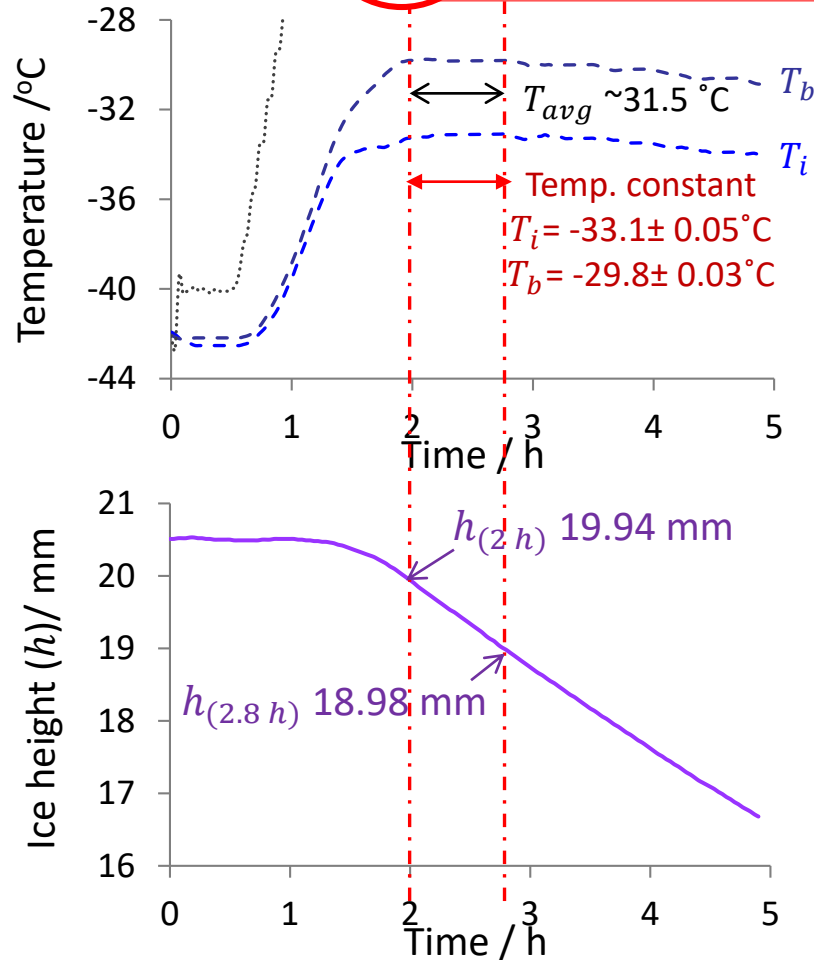
Cross-section area ( $A$ ) =  $3.80 \text{ cm}^2$

Ice height at 2 h ( $h_{(2h)}$ ) =  $19.94 \text{ mm}$

# Objective

## IX

Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t1)} - h_{(t2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920\text{ g}\cdot\text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

Internal vial diameter (VC010-20C) =  $2.21\text{ cm}$

Cross-section area ( $A$ ) =  $3.80\text{ cm}^2$

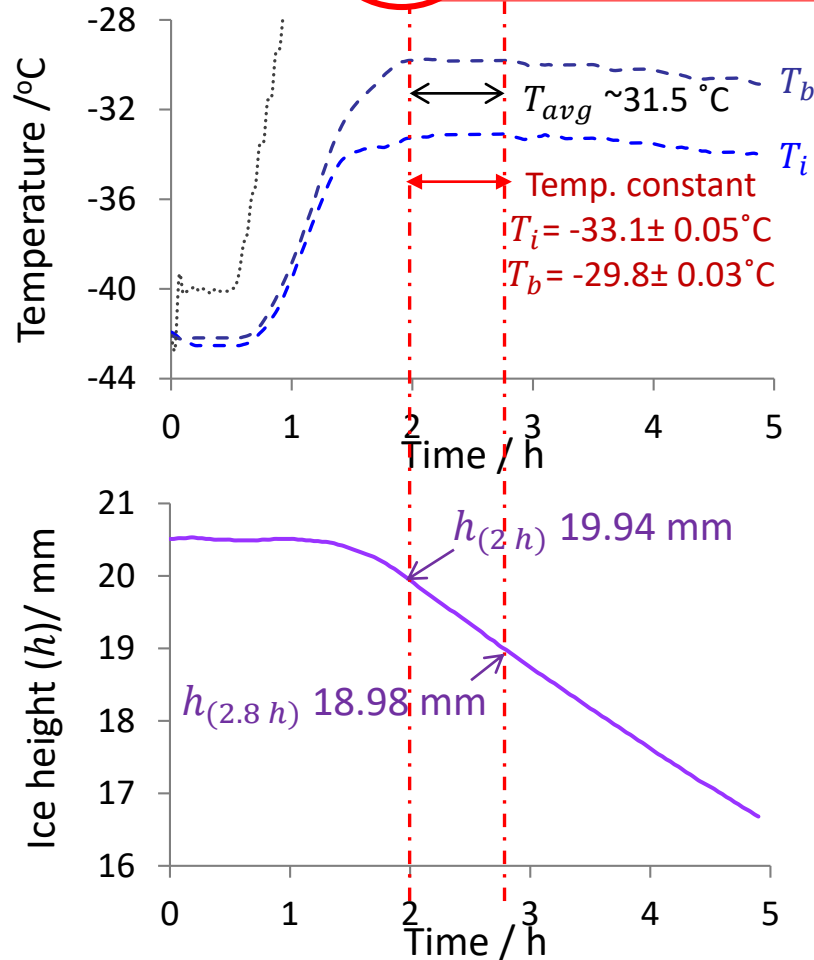
Ice height at 2 h ( $h_{(2\text{ h})}$ ) =  $19.94\text{ mm}$

Ice height at 2.8 h ( $h_{(2.8\text{ h})}$ ) =  $18.98\text{ mm}$

# Objective

IX

Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920 \text{ g} \cdot \text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

Internal vial diameter (VC010-20C) =  $2.21 \text{ cm}$

Cross-section area ( $A$ ) =  $3.80 \text{ cm}^2$

Ice height at  $2 \text{ h}$  ( $h_{(2h)}$ ) =  $19.94 \text{ mm}$

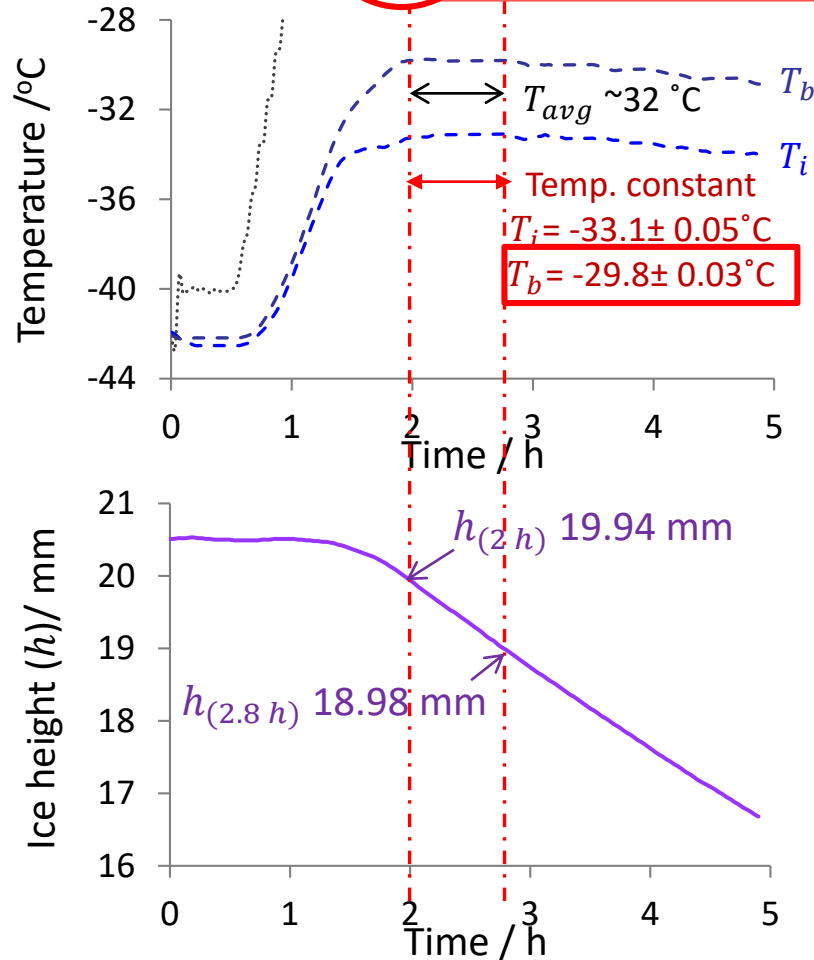
Ice height at  $2.8 \text{ h}$  ( $h_{(2.8h)}$ ) =  $18.98 \text{ mm}$

$$\begin{aligned} \text{Drying rate} &= 0.920 \text{ g} \cdot \text{cm}^{-3} \times 3.80 \text{ cm}^2 \times \frac{(19.94 - 18.98) \times 10^{-1} \text{ cm}}{(2.8 - 2.0) \text{ h}} \\ &= \mathbf{0.42 \text{ g} \cdot \text{h}^{-1}} \end{aligned}$$

# Objective

IX

Determination (i) the drying rate ( $\Delta m/\Delta t$ ) and (ii) ice base temperature ( $T_b$ ) during the steady state period for heat transfer coefficient ( $K_v$ ) calculation



- Drying rate during the steady state

$$\text{Drying rate } \left( \frac{\Delta m}{\Delta t} \right) = \rho_i \cdot A \cdot \frac{h_{(t_1)} - h_{(t_2)}}{t_2 - t_1}$$

Ice density ( $\rho_i$ ) at  $-32^\circ\text{C}$  =  $0.920\text{ g}\cdot\text{cm}^{-3}$

(Calculated ice temperature between  $T_i$  &  $T_b$ )

Internal vial diameter (VC010-20C) =  $2.21\text{ cm}$

Cross-section area (A) =  $3.80\text{ cm}^2$

Ice height at 2 h ( $h_{(2\text{ h})}$ ) =  $19.94\text{ mm}$

Ice height at 2.8 h ( $h_{(2.8\text{ h})}$ ) =  $18.98\text{ mm}$

TVIS parameters used for determination:

$$\frac{\Delta m}{\Delta t} = 0.42\text{ g}\cdot\text{h}^{-1}$$

$$T_b = -29.8^\circ\text{C}$$

$$\begin{aligned} \text{Drying rate} &= 0.920\text{ g}\cdot\text{cm}^{-3} \times 3.80\text{ cm}^2 \times \frac{(19.94 - 18.98) \times 10^{-1}\text{ cm}}{(2.8 - 2.0)\text{ h}} \\ &= \mathbf{0.42\text{ g}\cdot\text{h}^{-1}} \end{aligned}$$

## Objective

X

Heat transfer coefficient ( $K_v$ ) calculation

# Objective

X

Heat transfer coefficient ( $K_v$ ) calculation



| Parameters   | TVIS  |
|--|-------|
| Drying rate at steady state (g/h)<br>(2-2.8 h into primary drying) | 0.42  |
| Shelf Temperature, $T_s$ (K)                                       | 273.3 |
| Vial's base Temperature, $T_b$ (K)                                 | 243.3 |

# Objective X Heat transfer coefficient ( $K_v$ ) calculation

| Parameters   | TVIS  |
|--|-------|
| Drying rate at steady state (g/h)<br>(2-2.8 h into primary drying) | 0.42  |
| Shelf Temperature, $T_s$ (K)                                       | 273.3 |
| Vial's base Temperature, $T_b$ (K)                                 | 243.3 |

$$L \frac{\Delta m}{\Delta t} = A_e K_v (T_s - T_b) \Rightarrow K_v = \frac{L \frac{\Delta m}{\Delta t}}{A_e (T_s - T_b)}$$

$L$  is the latent heat of sublimation of ice ( $2844 \text{ J} \cdot \text{g}^{-1}$  or  $679.7 \text{ cal} \cdot \text{g}^{-1}$ ) and  $A_e$  is external cross-sectional area of the base of the TVIS vial ( $4.62 \text{ cm}^2$ )

*Pikal, et al. (1984)*



# Objective X Heat transfer coefficient ( $K_v$ ) calculation

| Parameters   | TVIS  |
|--|-------|
| Drying rate at steady state (g/h)<br>(2-2.8 h into primary drying) | 0.42  |
| Shelf Temperature, $T_s$ (K)                                       | 273.3 |
| Vial's base Temperature, $T_b$ (K)                                 | 243.3 |

$$L \frac{\Delta m}{\Delta t} = A_e K_v (T_s - T_b) \Rightarrow K_v = \frac{L \frac{\Delta m}{\Delta t}}{A_e (T_s - T_b)}$$

$L$  is the latent heat of sublimation of ice ( $2844 \text{ J} \cdot \text{g}^{-1}$  or  $679.7 \text{ cal} \cdot \text{g}^{-1}$ ) and  $A_e$  is external cross-sectional area of the base of the TVIS vial ( $4.62 \text{ cm}^2$ )

$$K_v(270 \mu\text{bar}) = \frac{L \frac{\Delta m}{\Delta t}}{A_e (T_s - T_b)}$$

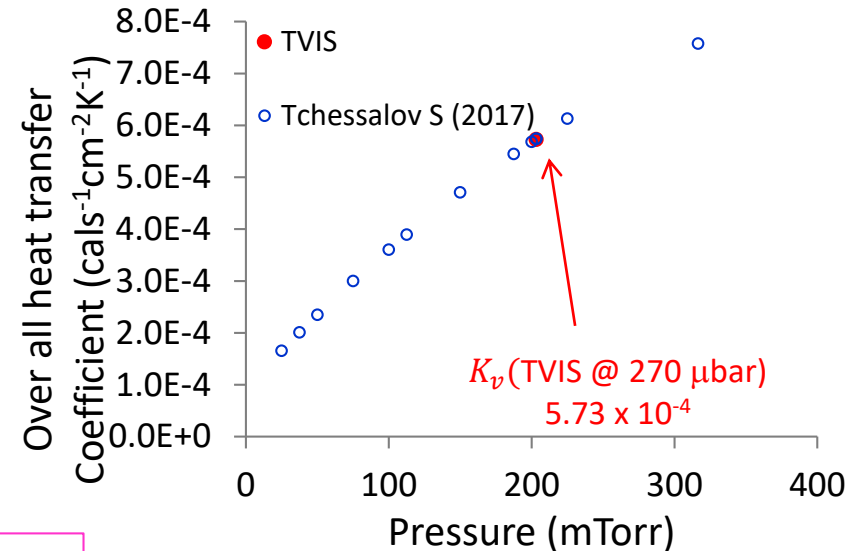
$$\begin{aligned} &= \frac{679.7 \text{ cal} \cdot \text{g}^{-1} \times 0.42 \text{ g} \cdot \text{h}^{-1}}{4.62 \text{ cm}^2 \times (273.3 - 243.3) \text{ K}} \\ &= 2.06 \text{ cal} \cdot \text{h}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1} \\ &= 5.73 \times 10^{-4} \text{ cal} \cdot \text{s}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1} \end{aligned}$$

Pikal, et al. (1984)

$$K_v(270 \mu\text{bar}) = 5.73 \times 10^{-4} \text{ cal} \cdot \text{s}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1}$$

# Objective X Heat transfer coefficient ( $K_v$ ) calculation

| Parameters   | TVIS  |
|--|-------|
| Drying rate at steady state (g/h)<br>(2-2.8 h into primary drying) | 0.42  |
| Shelf Temperature, $T_s$ (K)                                       | 273.3 |
| Vial's base Temperature, $T_b$ (K)                                 | 243.3 |



$$L \frac{\Delta m}{\Delta t} = A_e K_v (T_s - T_b) \Rightarrow$$

$$K_v = \frac{L \frac{\Delta m}{\Delta t}}{A_e (T_s - T_b)}$$

$L$  is the latent heat of sublimation of ice (2844 J·g<sup>-1</sup> or 679.7 cal·g<sup>-1</sup>) and  $A_e$  is external cross-sectional area of the base of the TVIS vial (4.62 cm<sup>2</sup>)

$$K_v(270 \mu\text{bar}) = \frac{L \frac{\Delta m}{\Delta t}}{A_e (T_s - T_b)}$$

$$\begin{aligned}
 &= \frac{679.7 \text{ cal} \cdot \text{g}^{-1} \times 0.42 \text{ g} \cdot \text{h}^{-1}}{4.62 \text{ cm}^2 \times (273.3 - 243.3) \text{ K}} \\
 &= 2.06 \text{ cal} \cdot \text{h}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1} \\
 &= 5.73 \times 10^{-4} \text{ cal} \cdot \text{s}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1}
 \end{aligned}$$

Pikal, et al. (1984)

$$K_v(270 \mu\text{bar}) = 5.73 \times 10^{-4} \text{ cal} \cdot \text{s}^{-1} \cdot \text{cm}^{-2} \cdot \text{K}^{-1}$$

# Additional comments



Qualification of steady state heat transfer mechanisms

# A single vial technique

Pikal, et al. (1984)

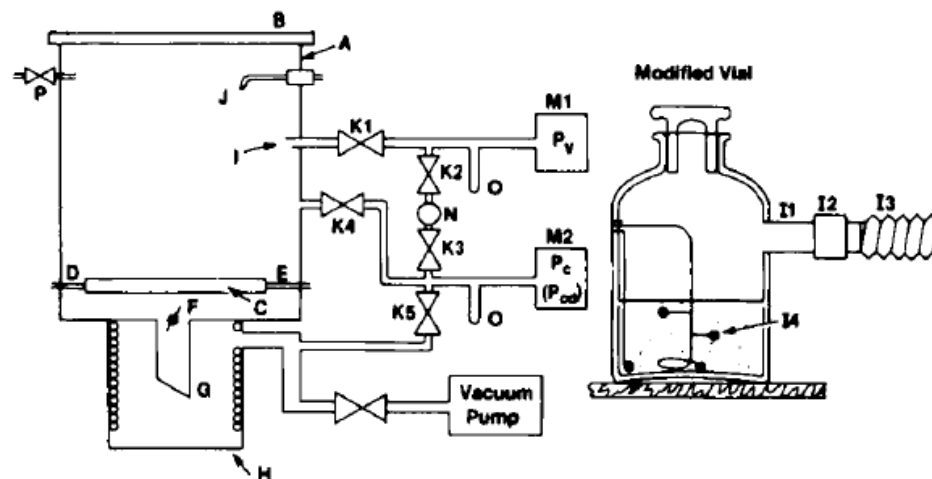


Figure 1—Schematic of the laboratory freeze-dryer (see text for key).

The mean sublimation rate was calculated from the mass of ice sublimed and the time required for sublimation.

Table IV—Evaluation of Heat Transfer by Top Radiation: Effective Emissivity,  $e_v$

| Product           | $N$ | $A_v$ | $e_v \pm \sigma_m$ |
|-------------------|-----|-------|--------------------|
| H <sub>2</sub> O  | 7   | 4.71  | $0.83 \pm 0.04$    |
| H <sub>2</sub> O  | 3   | 6.83  | $0.94 \pm 0.02$    |
| H <sub>2</sub> O  | 3   | 17.2  | $0.79 \pm 0.03$    |
| KCl ( $I = 0$ )   | 2   | 4.71  | 0.88               |
| KCl ( $I = 0.3$ ) | 1   | 4.71  | 0.97               |
| KCl ( $I = 0$ )   | 1   | 20.8  | 0.58               |
| KCl ( $I = 0.2$ ) | 1   | 20.8  | 0.80               |
| Mean              |     |       | 0.84               |

currer such that ice near the vial wall and ice near the thermocouple wire was preferentially removed. As a result of this phenomenon, measurements of temperature distribution in the ice had to be completed early in the experiment, before the assumption of a planar ice-vapor interface was seriously violated. Accurate temperature distribution data was obtained until ~15% of the ice had been removed. The vial heat transfer coefficient is defined assuming the ice at the vial bottom is in good thermal contact with the glass. Normally, with vials filled with pure water, partial loss of thermal contact occurs after sublimation of 35–50% of the ice. Thus, duration of a heat transfer experiment is limited to a time corresponding to sublimation of ~25% of the ice. Loss of thermal contact is rarely a problem when a frozen solution is dried.

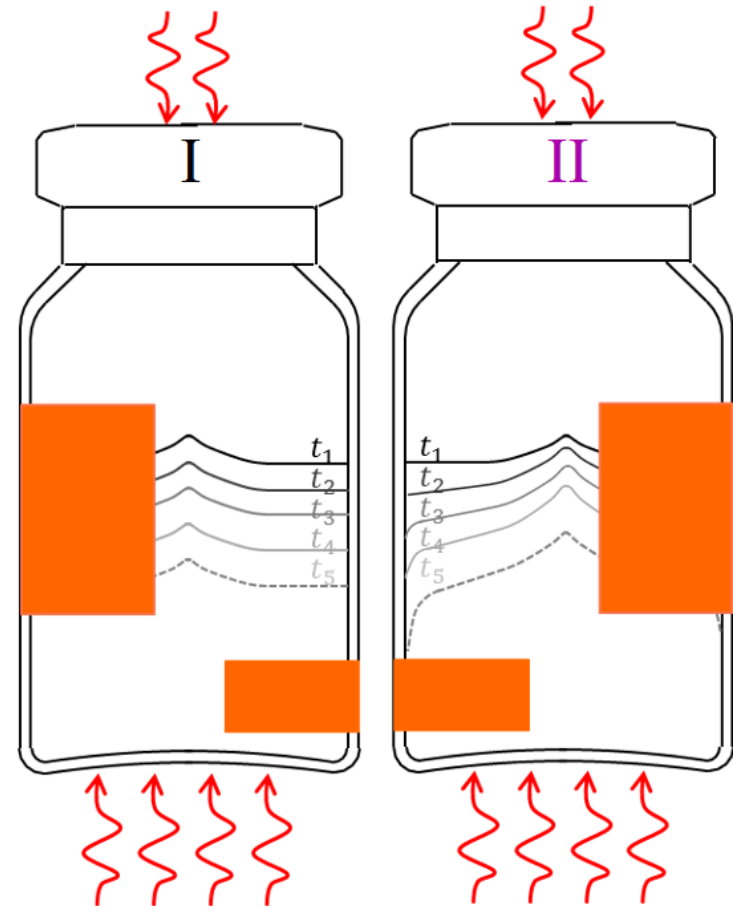
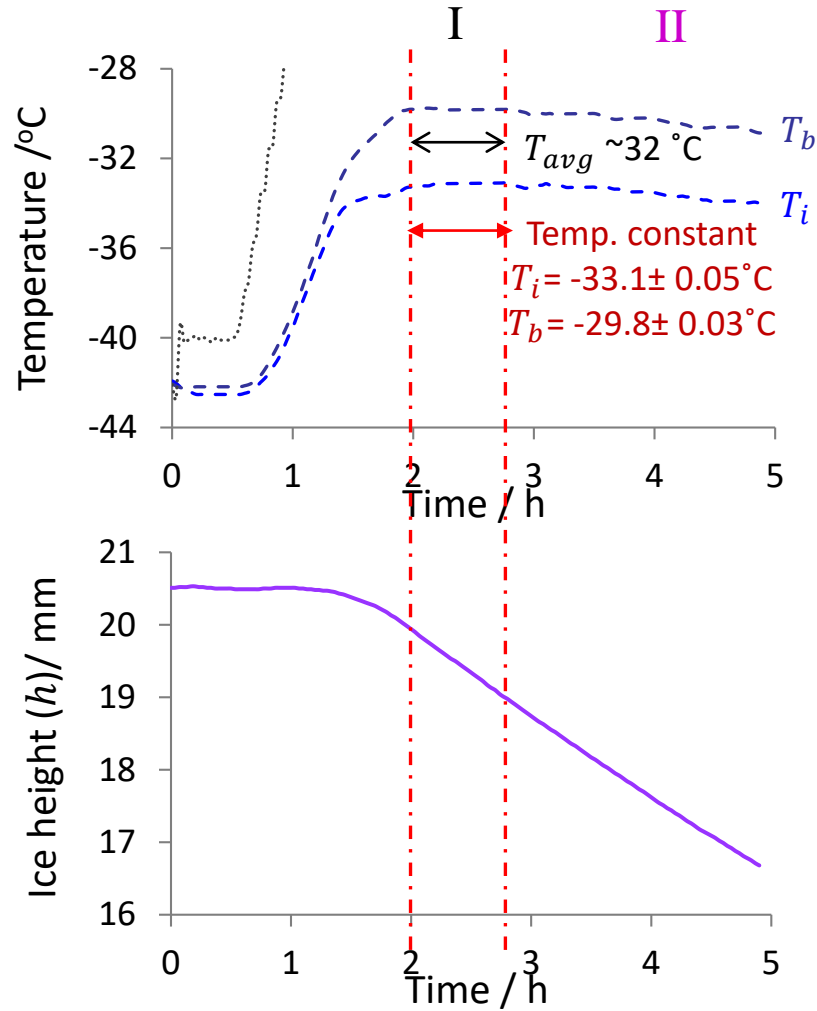
For single vial heat transfer studies, a representative vial from a given lot of vials was modified as shown in Fig. 1. After filling, normally with pure water, the modified vial and other vials of the same lot, all equipped with "identical" metal tubes, were loaded into the laboratory dryer, the liquid was frozen, and the chamber was evacuated. The procedure then involved a series of heat transfer measurements under steady-state conditions at selected shelf temperatures and chamber pressures. An operational definition of steady state is taken as constant temperatures ( $\pm 0.2^\circ\text{C}$ ) and pressures ( $\pm 2 \mu\text{m}$ ) for a period of 10–15 min. The sublimation rate,  $\dot{m}$ , is calculated from the observed steady-state pressure readings using Eq. 3 with the closure resistance given by the tube resistance, Eq. 17. The heat transfer rate,  $\dot{Q}$ , is then calculated:

$$\dot{Q} \text{ (cal/s)} = 0.1833\dot{m} \text{ (g/h)} \quad (\text{Eq. 18})$$

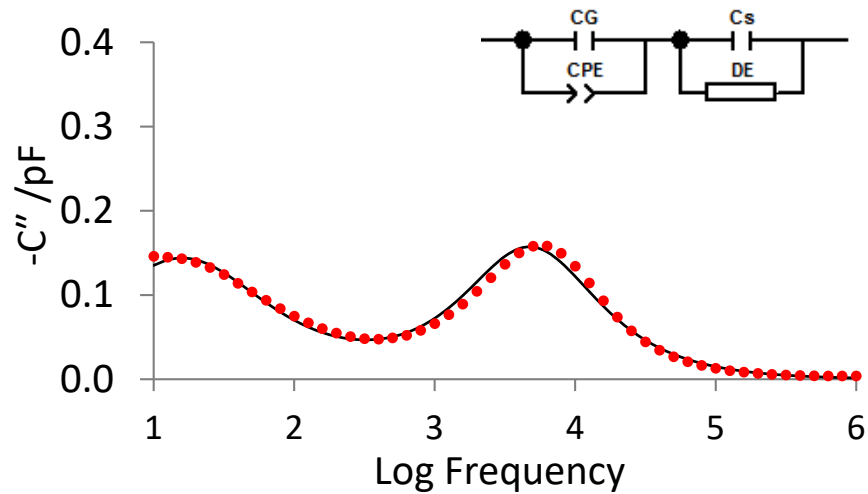
# Assumption for $K_v$ determination

- How do we know that the heat transfer mechanisms are constant up to 25% loss of ice mass?
- If the heat transfer mechanisms change because of ice- glass interface contact or because of the change of ice shape (surface area) then surely heat transfer coefficient will change?
- It requires a technique to qualify when the heat transfer mechanisms change
- So can TVIS demonstrate when ice leaves the glass wall interface?

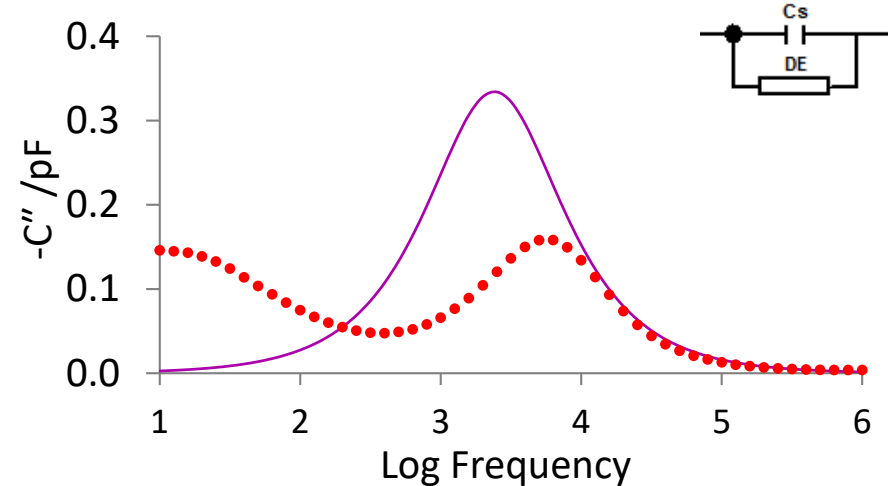
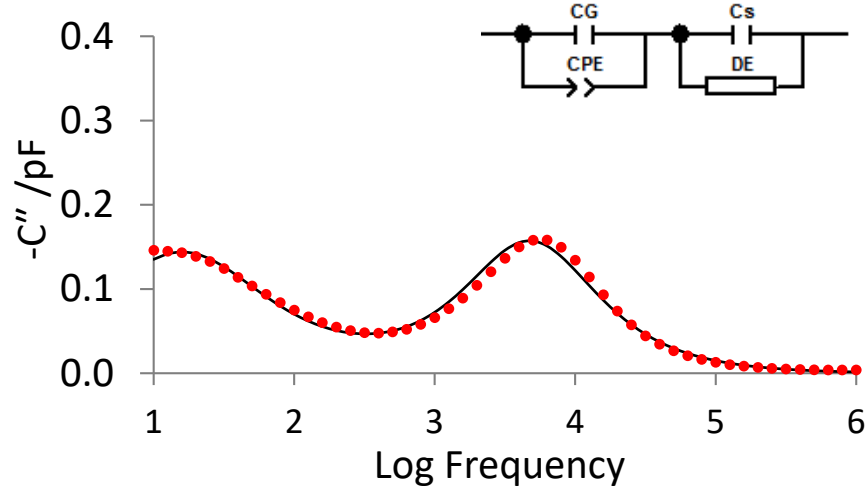
# Limitation of TVIS System ?



# Limitation of TVIS System ?



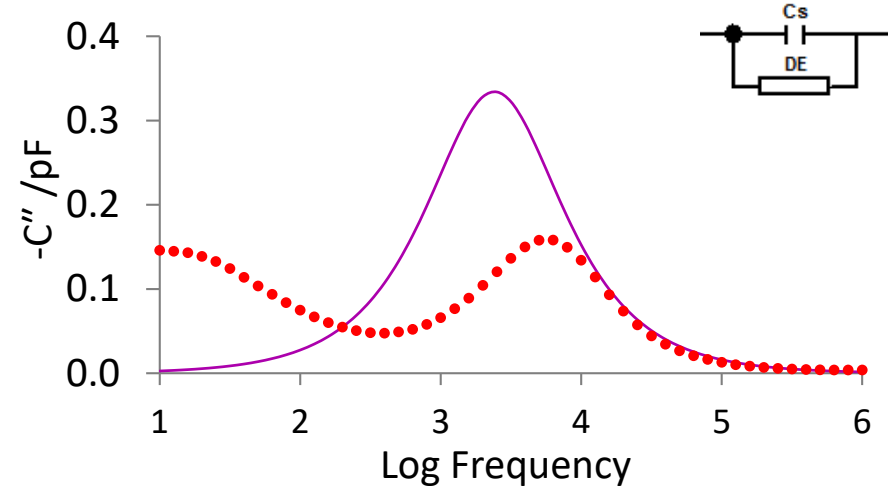
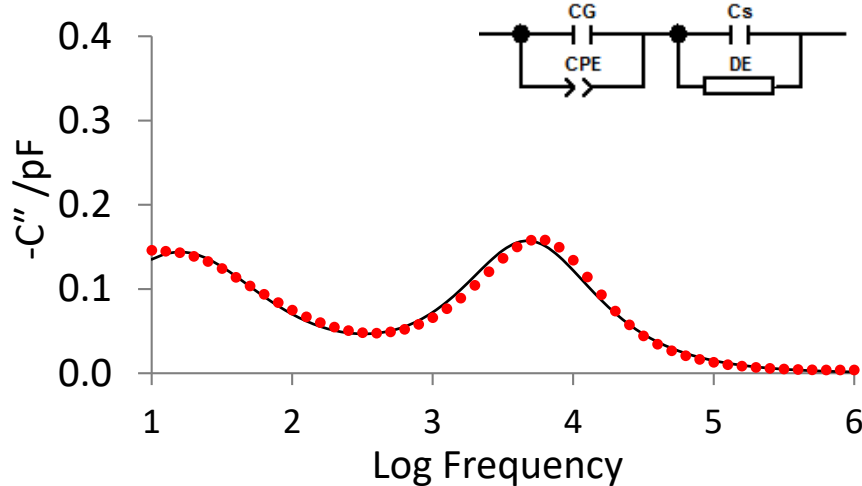
# Limitation of TVIS System ?



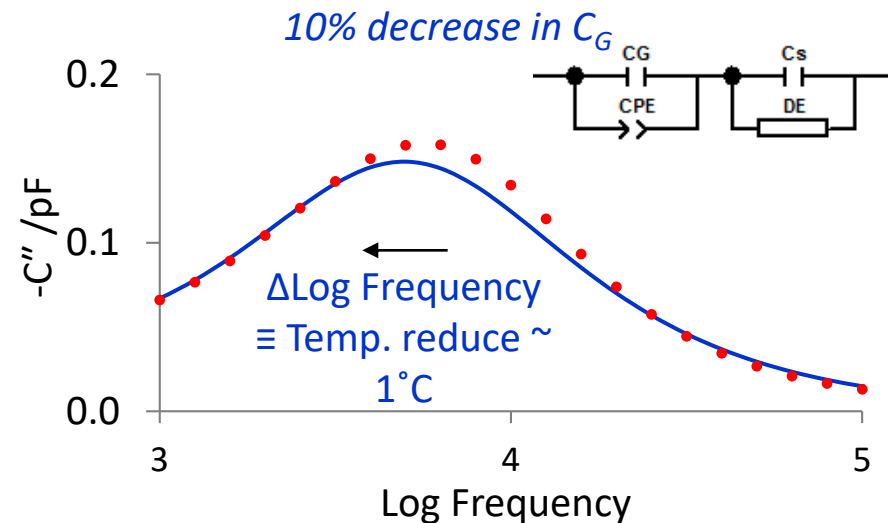
- Glass wall impedance increase the peak frequency ( $F_{PEAK}$ ) but reduce the peak amplitude ( $C''_{PEAK}$ )



# Limitation of TVIS System ?



- Glass wall impedance increase the peak frequency ( $F_{PEAK}$ ) but reduce the peak amplitude ( $C''_{PEAK}$ )
- Decrease in  $F_{PEAK}$  during primary drying is due to loss of contact of ice with the side wall



## Discussion

- Decrease in  $F_{PEAK}$  suggests that the temperature may be decreasing after the steady state period, contrary to accepted knowledge that the temperature starts to increase owing to a reduction in drying rate and hence the degree of self cooling
- Decrease in  $F_{PEAK}$  is more likely to be due to a change in the ice-glass contact associated with a change in the shape of the ice cylinder.

## Conclusion

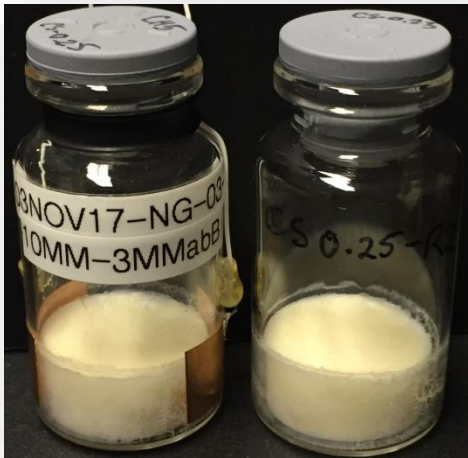
- The period for determining the drying rate should be decreased from 25% ice loss to 10% for TVIS to give reliable estimates for  $K_v$
- Opportunity to cycle through shelf temperature and chamber pressure to create the design space for  $K_v$  determinations as a function of shelf position.

# Limitations

- $C''_{PEAK}$  and  $F_{PEAK}$  parameters rely on intimate contact of ice cylinder with glass wall
- $C'(100\text{ kHz})$  parameter does not depend on contact and can be used for end point but relationship between  $C'(100\text{ kHz})$  ice constant is non-linear
- Cable length limited to 1m at present
- C-TVIS not compatible with front loading system
- Incompatible with TCs in same TVIS vial (use fibre optic sensors – INFAP)

# Future Work

- Development dryer mapping of sublimation characteristics
  - heat transfer coefficients ( $K_V$ )
  - dry layer resistance ( $R_P$ )



- Instrument Development
  - Contact C-TVIS instrument (2018)
  - Non-contact TVIS (2018-19)
    - Micro-well screening
    - Vial clusters in batch FD
  - TVIS - Shuttle (2019-20)

# Acknowledgements, Recent Projects & Collaborators

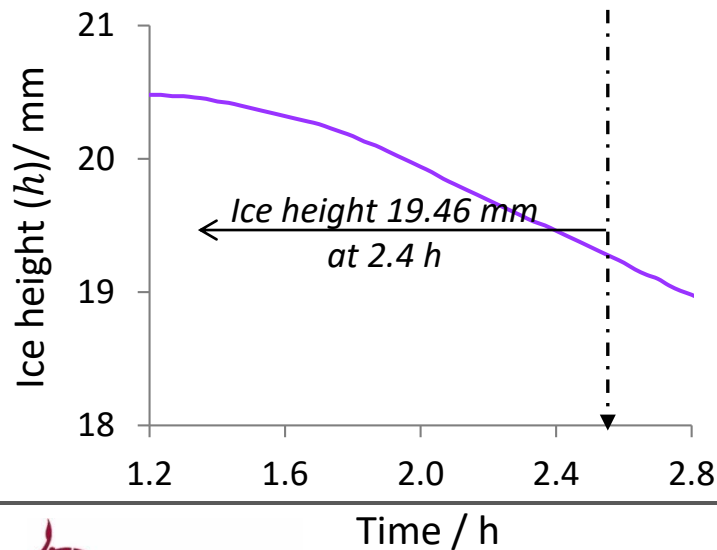
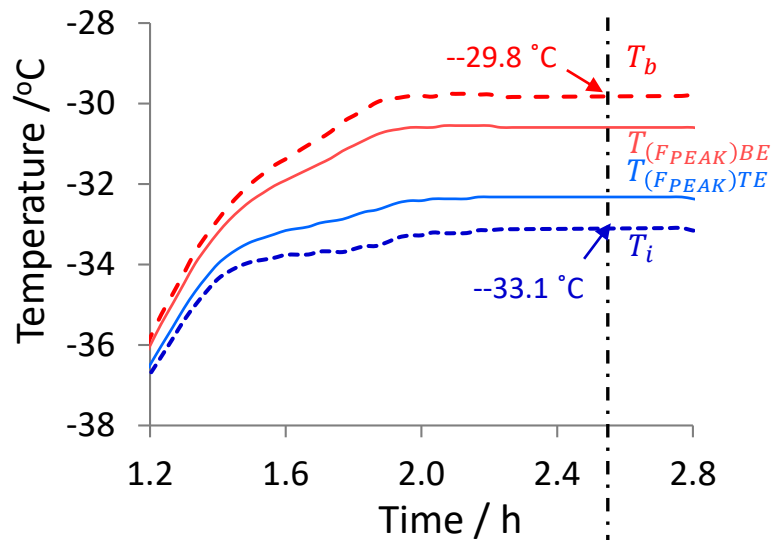
- De Montfort University, School of Pharmacy
  - Evgeny Polygalov: co-inventor of TVIS instrument
  - Yowwares Jeeraruangrattana. PhD student
  - Bhaskar Pandya. PhD student
  - Irina Ermolina. Senior Lecturer



Through Vial Impedance Spectroscopy



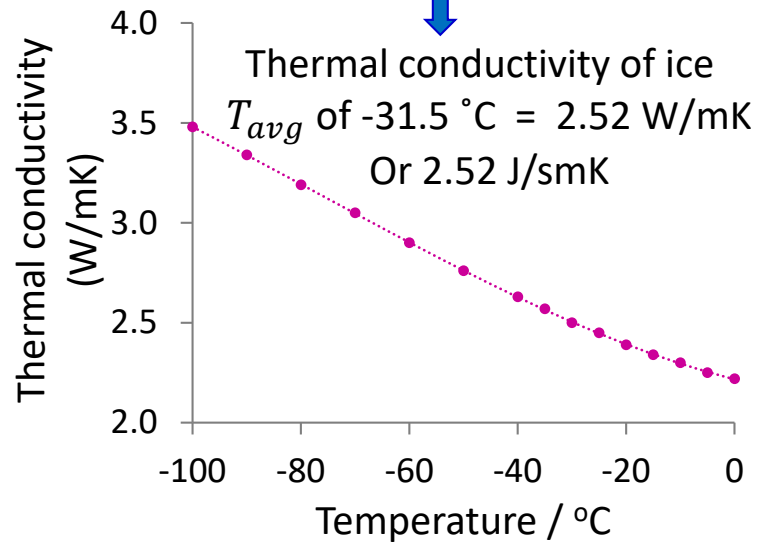
Thank you



| Parameters   | TVIS   |
|--|--------|
| Ice interfacial temperature, $T_i$ (K)                       | 240.1  |
| Vial's base Temperature, $T_b$ (K)                           | 243.3  |
| Ice height or thickness of material, $d$ (m)                 | 0.0195 |
| Average temperature (between $T_i$ & $T_b$ ), $T_{avg}$ (°C) | -31.5  |
| $\Delta T$ (between $T_i$ & $T_b$ ) (K)                      | 3.3    |

## Objective

$$y = 4E-07x^2 - 0.0001x^2 - 0.0069x + 2.2174$$



### Parameters

| Parameters   | TVIS   |
|--|--------|
| Ice interfacial temperature, $T_i$ (K)                       | 240.1  |
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| $\Delta T$ (between $T_i$ & $T_b$ ) (K)                      | 3.3    |

$$\text{Drying rate } \left(\frac{\Delta m}{\Delta t}\right) = \frac{kA\Delta T}{Ld}$$



$$\frac{\Delta m}{\Delta t} = \frac{2.52\text{ W} \cdot \text{m}^{-1}\text{K}^{-1} \times 0.00038\text{ m}^2 \times 3.3\text{ K}}{2844 \times 0.0195}$$

$$= \frac{2.52\text{ J} \cdot \text{s}^{-1}\text{m}^{-1}\text{K}^{-1} \times 0.00038\text{ m}^2 \times 3.3\text{ K}}{2844\text{ J} \cdot \text{g}^{-1} \times 0.0195\text{ m}}$$

$$= 5.74 \times 10^{-5}\text{ g/s}$$

$$= 0.207\text{ g/h}$$

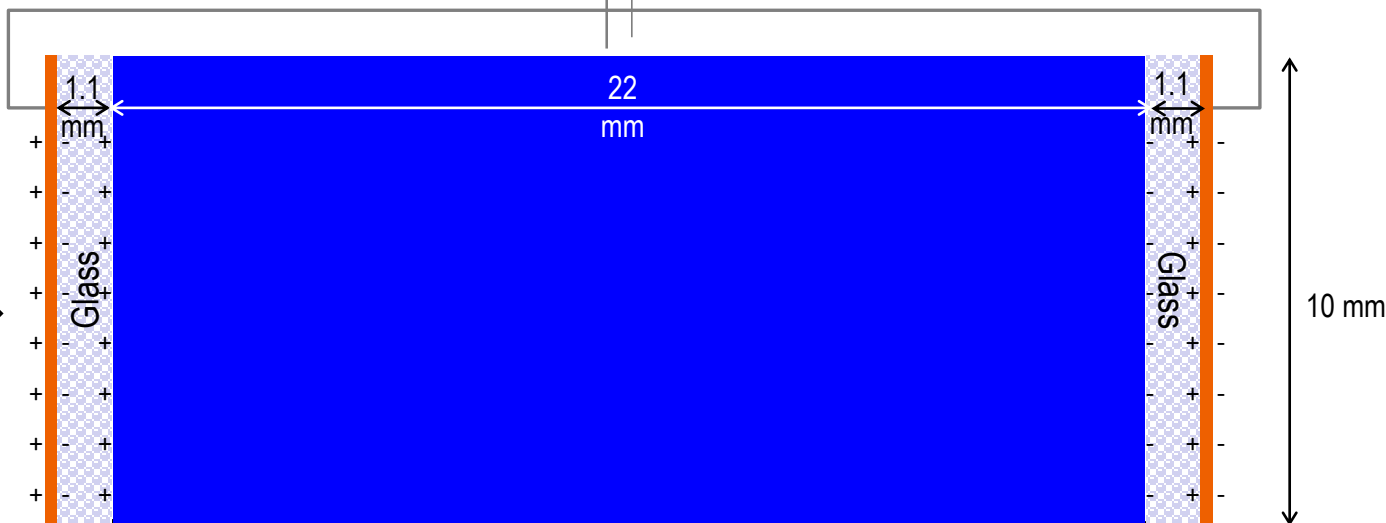
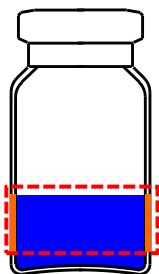
$k$  is the thermal conductivity constant for the material  
 $A$  is the cross sectional area of the material transferring heat ( $\equiv$  internal cross-sectional area of vial)  $0.00038\text{ m}^2$   
 $\Delta T$  is the difference in temperature between one side of the material and the other  
 $L$  is Latent heat of sublimation at 240 K ( $2844\text{ J/g}$ )  
 $d$  is the thickness of the material ( $\equiv$  ice height)



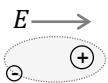
# Through Vial Impedance Spectroscopy (TVIS)

## *Dielectric Loss Mechanisms*

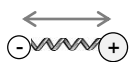
Measurement vial



**Electronic polarization**  
distortion of electrons  
relative to the nuclei

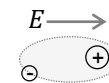


**Atomic polarization**  
distortion of nuclei across  
a heteroatom bond by  
stretching and bending

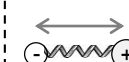


**Instantaneous polarization dominant  
mechanism in the glass wall**

**Electronic polarization**  
distortion of electrons  
relative to the nuclei

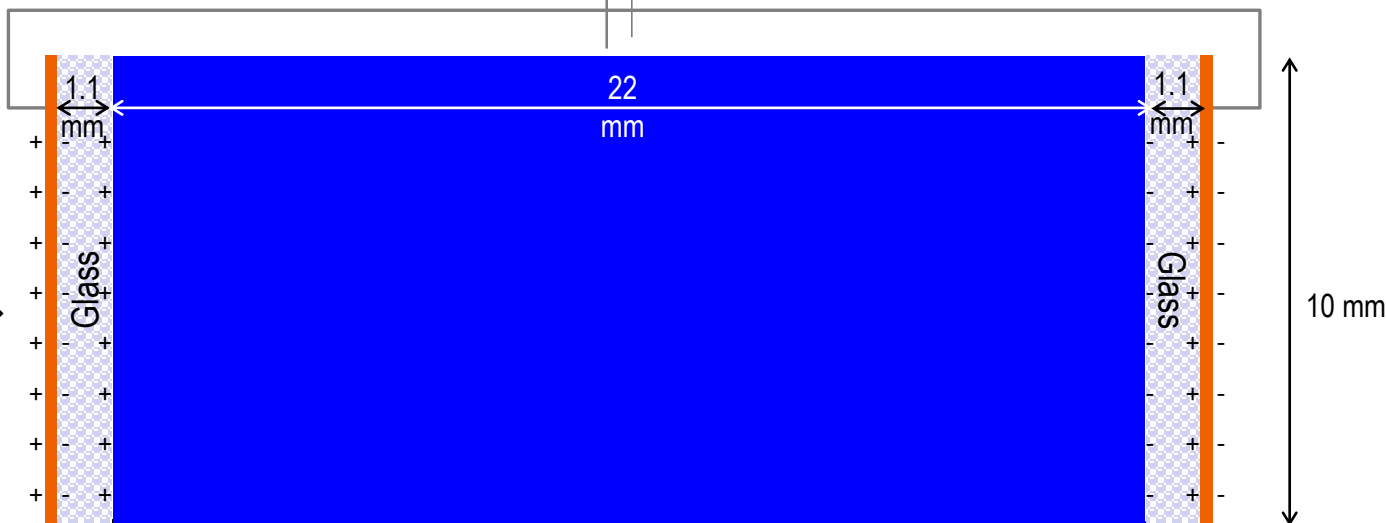
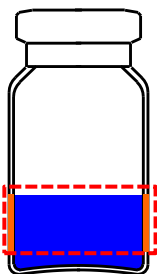


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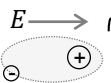


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Measurement vial



**Electronic polarization**  
distortion of electrons  
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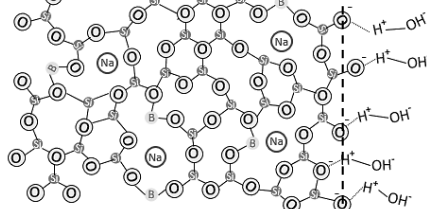


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stretching and bending



OH-  
OH-  
OH-  
OH-

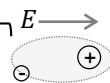
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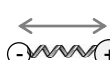
**Space charge polarization  
(weak frequency dependence)**

## MW (space-charge) polarization at glass wall – sample interface

**Electronic polarization**  
distortion of electrons  
relative to the nuclei

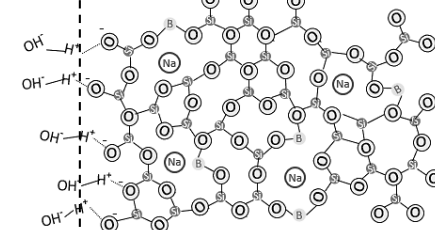


**Atomic polarization**  
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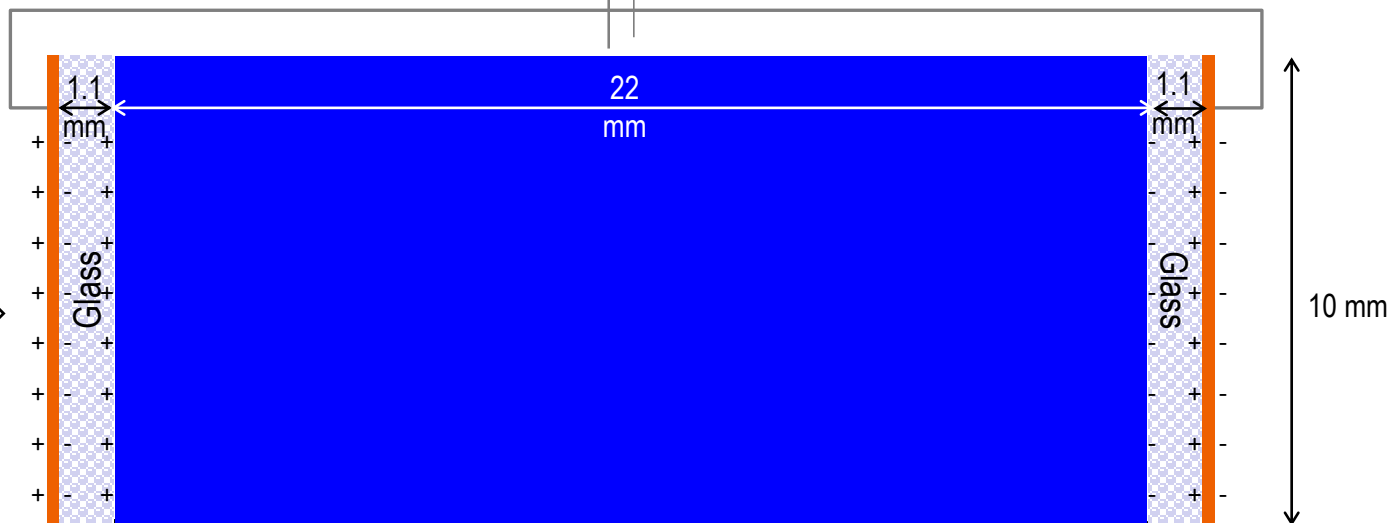
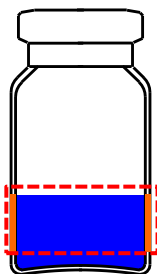
H+  
H+  
H+  
H+

**Instantaneous polarization dominant  
mechanism in the glass wall**

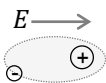


**Space charge polarization  
(weak frequency dependence)**

Measurement vial



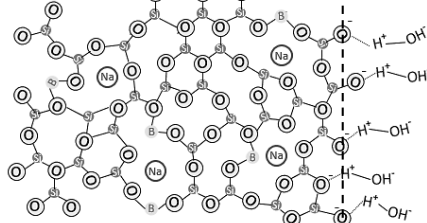
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**Atomic polarization**  
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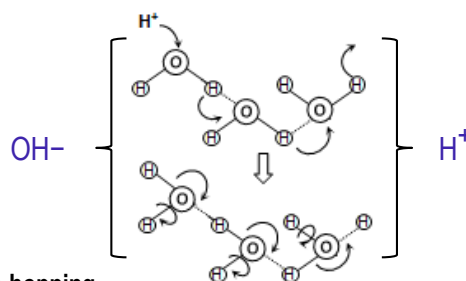


**Instantaneous polarization dominant  
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**Space charge polarization  
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**MW (space-charge) polarization at glass  
wall – sample interface**



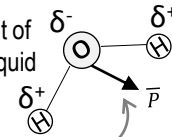
**Proton-hopping**

Conduction of protons in liquid water occurs  
through the Grotthuss "hop-turn" mechanism

**Conductivity in pure water**

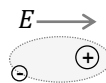
**Dipolar polarization**

re-orientation/alignment of  
permanent dipoles in liquid  
water (Debye-like  
relaxation)

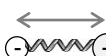


**Dielectric relaxation time,  
 $\tau \sim 9$  ps at 20°C)**

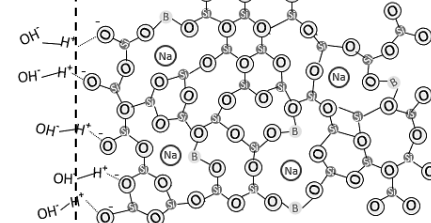
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stretching and bending



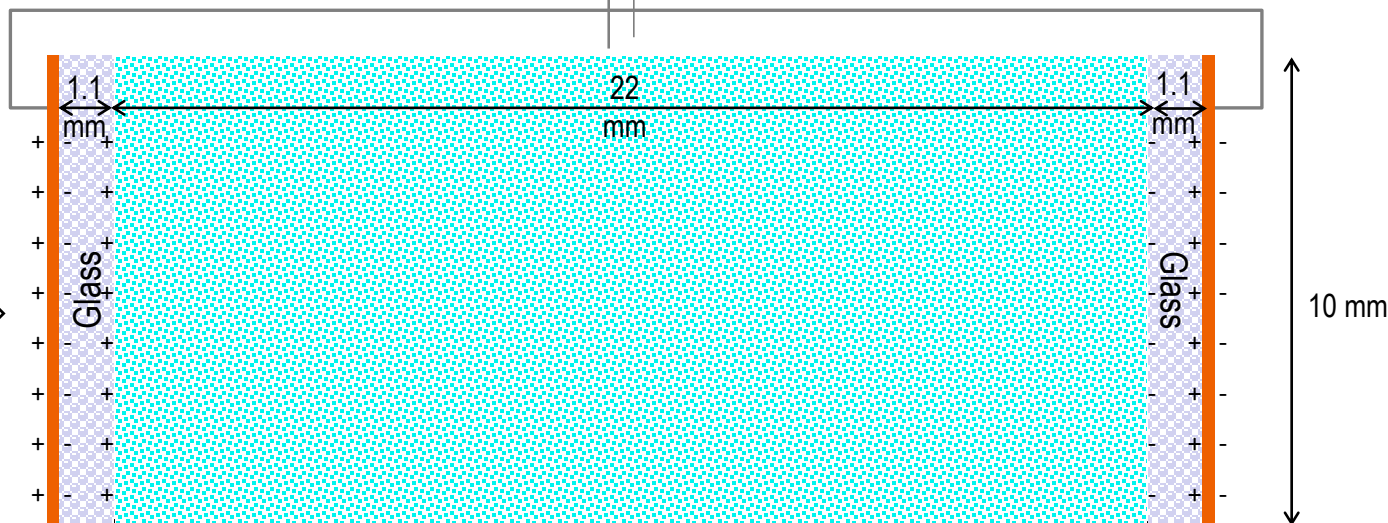
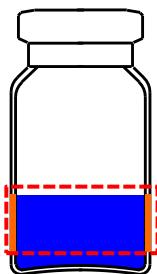
**Instantaneous polarization dominant  
mechanism in the glass wall**



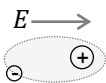
**Space charge polarization  
(weak frequency dependence)**

**MW (space-charge) polarization at glass  
wall – sample interface**

Measurement vial



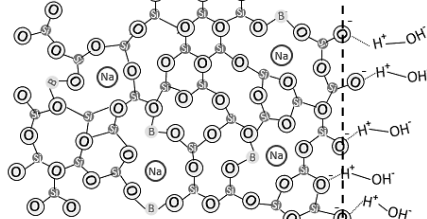
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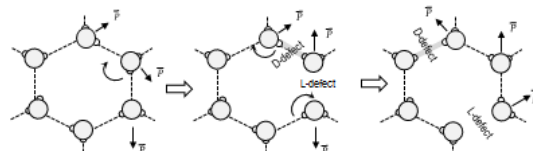
**Instantaneous polarization dominant  
mechanism in the glass wall**



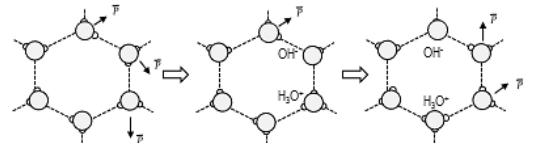
**Space charge polarization  
(weak frequency dependence)**

**MW (space-charge) polarization at glass  
wall – sample interface**

**Dominant at  $T > 235$  K (approx.  $-40$  °C)**  
Generation/migration of L- and D- orientation defects  
in ice Ih

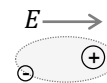


**Dominant at  $T < 235$  K (approx.  $-40$  °C)**  
Generation/migration of  $\text{H}_3\text{O}^+$ / $\text{OH}^-$  ion pairs (ionic  
defects) in ice Ih (similar to the Grotthus mechanism)



**Polarization mechanism in ice**

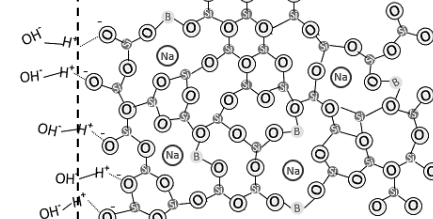
**Electronic polarization**  
distortion of electrons  
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**Atomic polarization**  
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**Instantaneous polarization dominant  
mechanism in the glass wall**

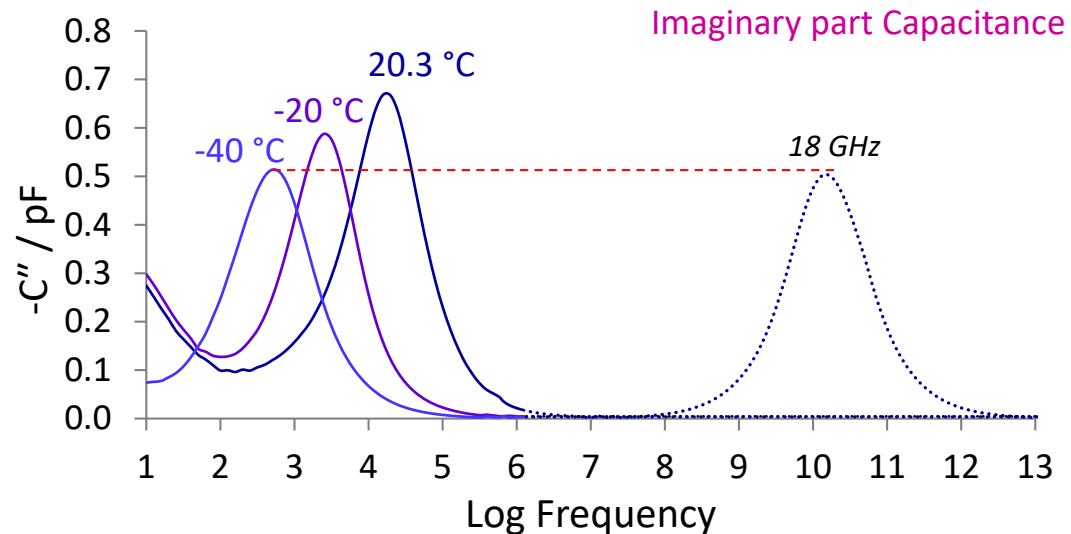
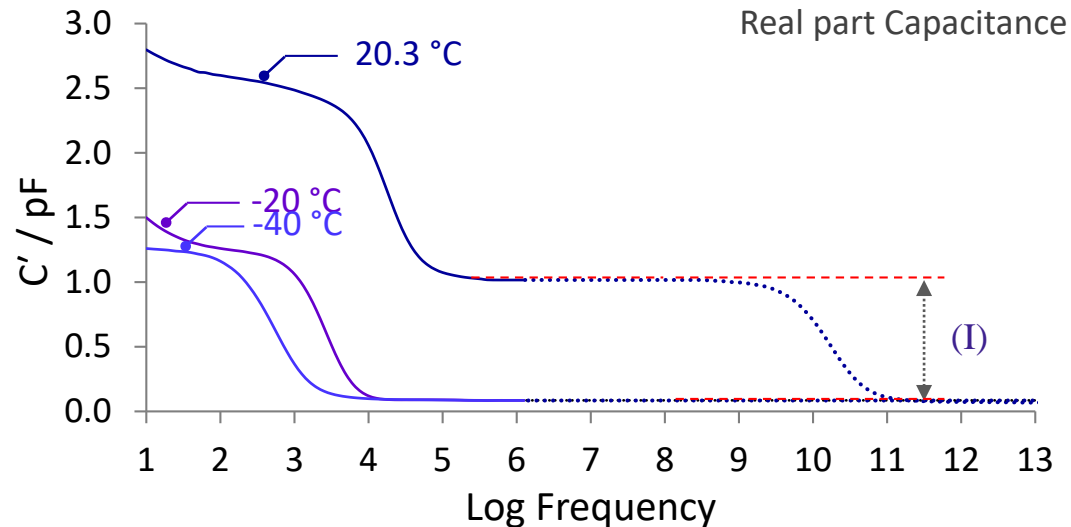


**Space charge polarization  
(weak frequency dependence)**

**MW (space-charge) polarization at glass  
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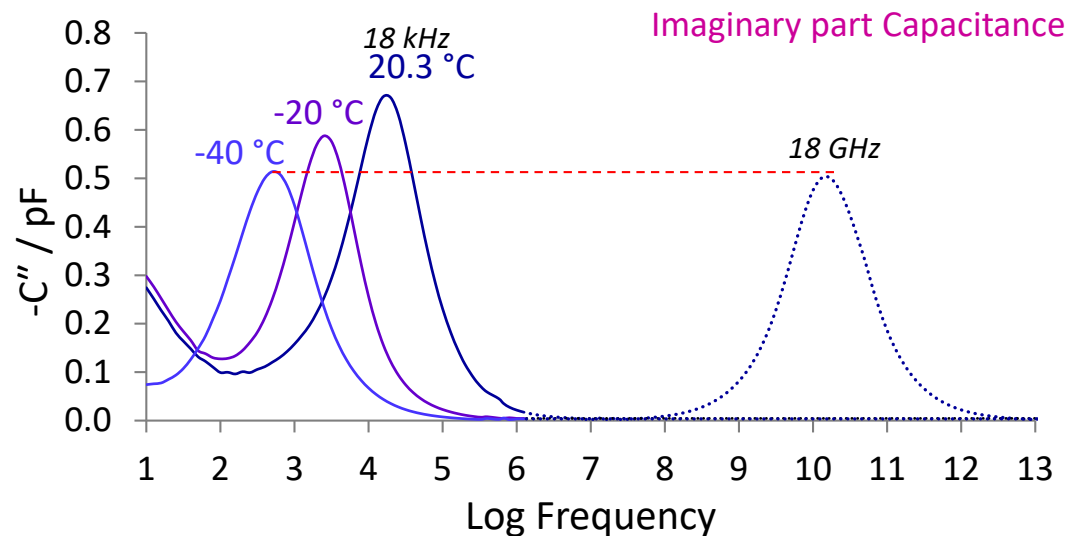
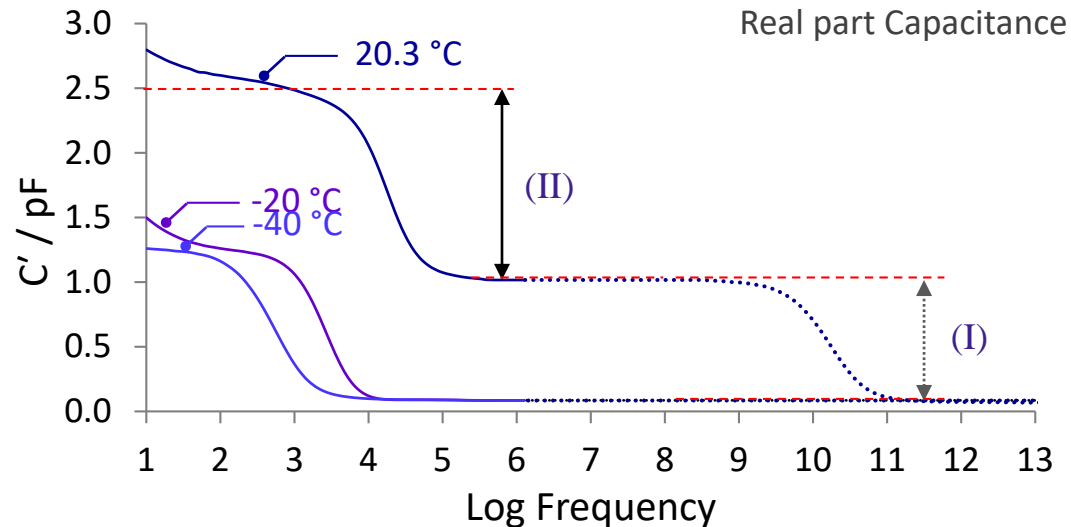
# Frozen Water and Dielectric Relaxation of Ice

- I. : The polarization of the water dipole in liquid water at 20 °C, with a dielectric loss peak frequency of ~ 18 GHz



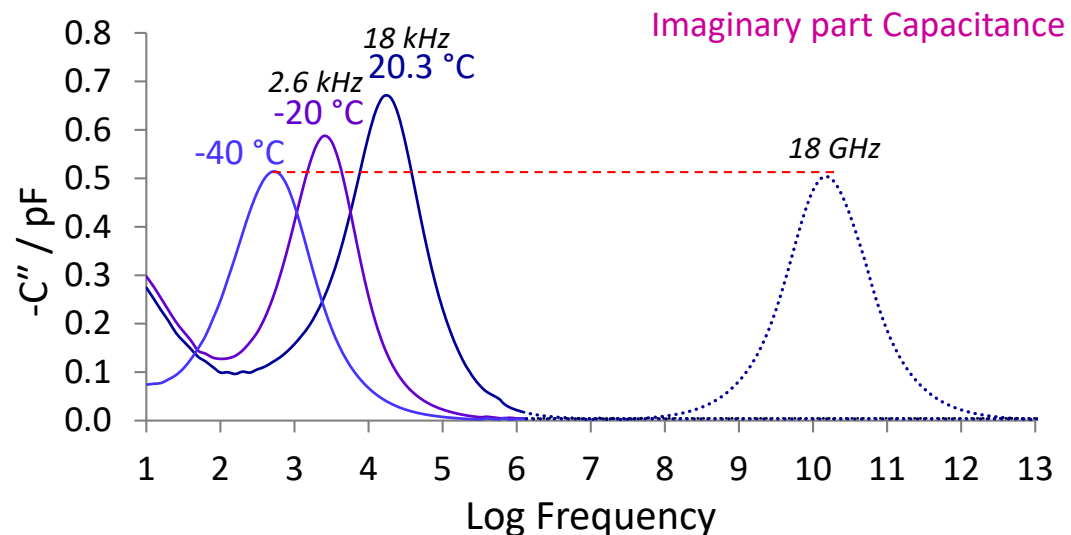
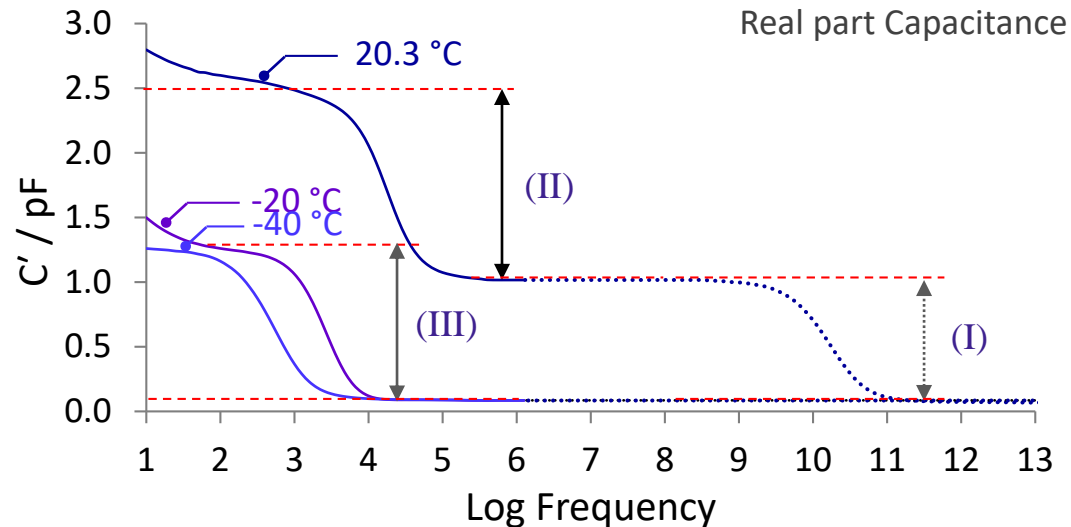
# Frozen Water and Dielectric Relaxation of Ice

- I. : The polarization of the water dipole in liquid water at 20 °C, with a dielectric loss peak frequency of ~ 18 GHz
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# Frozen Water and Dielectric Relaxation of Ice

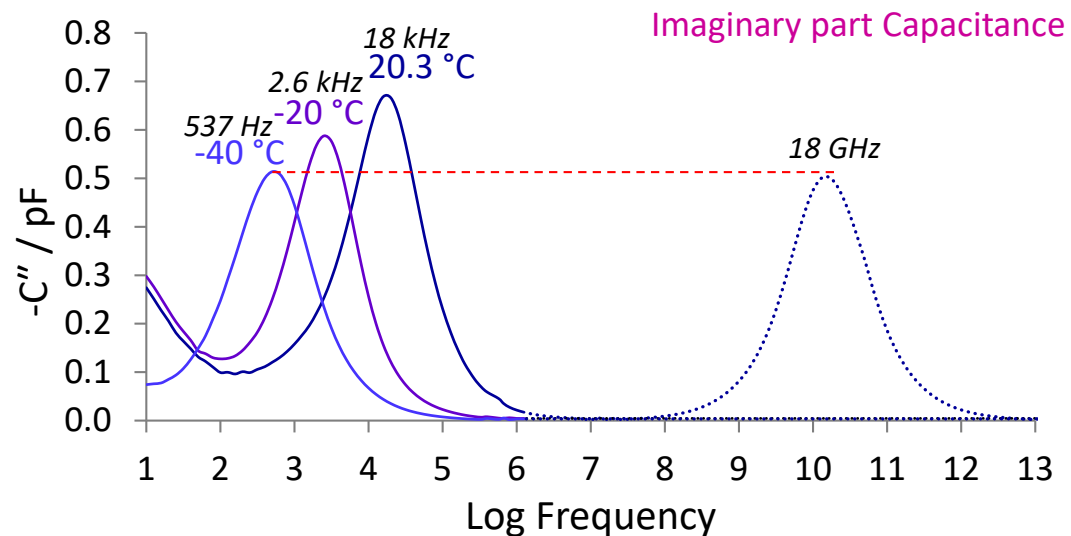
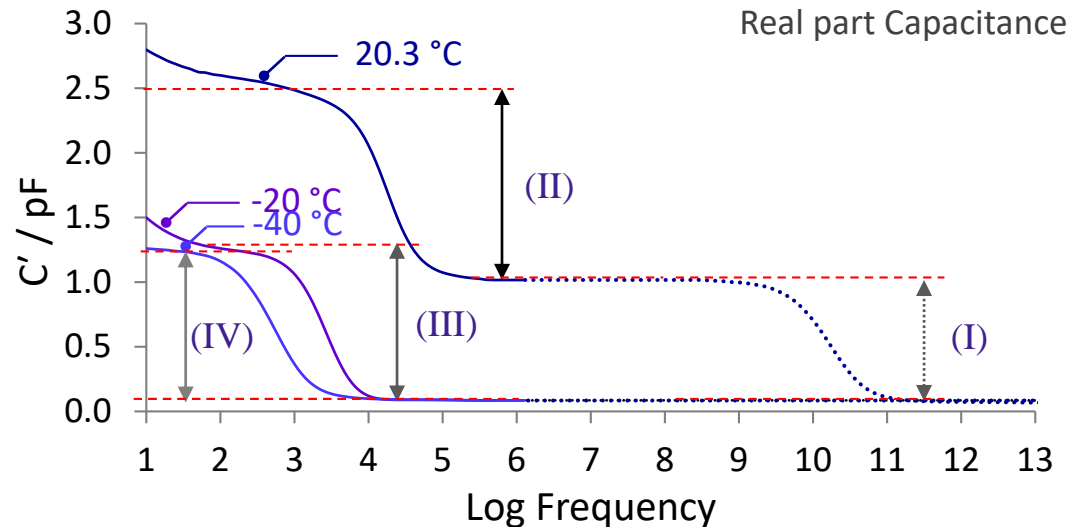
- I. : The polarization of the water dipole in liquid water at 20 °C, with a dielectric loss peak frequency of ~ 18 GHz
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- III. : The dielectric polarization of ice at -20 °C, with a dielectric loss peak frequencies of 2.57 kHz





# Frozen Water and Dielectric Relaxation of Ice

- I. : The polarization of the water dipole in liquid water at 20 °C, with a dielectric loss peak frequency of ~ 18 GHz
- II. : The Maxwell-Wagner (MW) polarization of the glass wall of the TVIS vial at 20 °C, with a dielectric loss peak frequency of 17.8 kHz
- III. : The dielectric polarization of ice at -20 °C, with a dielectric loss peak frequencies of 2.57 kHz
- IV. : The dielectric polarization of ice at -40 °C with a dielectric loss peak frequencies of 537 Hz.



# A single vial technique

Scutella et al. 2017

## Ice Sublimation Experiments

All experiments were performed using a 1.8-mL fill volume of distilled water (filling height: 11 mm). No stopper was inserted into the vial neck. The middle shelf was fully covered by filled vials for all runs, corresponding to a total of 540 vials in LYO A and 950 vials in LYO B. Bottomless trays were used.

The vials were quickly loaded on the pre-cooled shelf at  $-50^{\circ}\text{C}$ . The presence of a dry laminar flow in front of the freeze-dryer door made it possible to control the air relative humidity and thus to limit condensation on the shelves. After a freezing step of 2 h, the pressure was decreased and the shelf temperature was increased by  $1^{\circ}\text{C}/\text{min}$ . Experiments were carried out at 4, 6, 9, 15, 40, and 50 Pa with a shelf fluid inlet temperature of  $0^{\circ}\text{C}$ , and at 4 and 6 Pa with a shelf fluid inlet temperature of  $-40^{\circ}\text{C}$ . The run performed at  $0^{\circ}\text{C}$  and 6 Pa was repeated 3 times. The cycles were run long enough to dry up to 20%-25% of the initial fill volume. Subliming a larger quantity of ice could lead to loss of contact between the vial and the ice, introducing uncertainty in the analysis.

The sublimation rate  $\dot{m}$  was measured gravimetrically for each vial and calculated as the mass loss divided by the period of sublimation. A total of 100 vials, placed in the center of the shelf and surrounded by other vials in the same conditions, were individually weighed before and after the experiment on a precision scale ( $\pm 0.001$  g; Mettler Toledo, Zaventem, Belgium). Sublimation time was measured from the moment when shelf fluid inlet temperature exceeded product temperature, meaning that there was a net heat flux from the shelf toward the vials. The

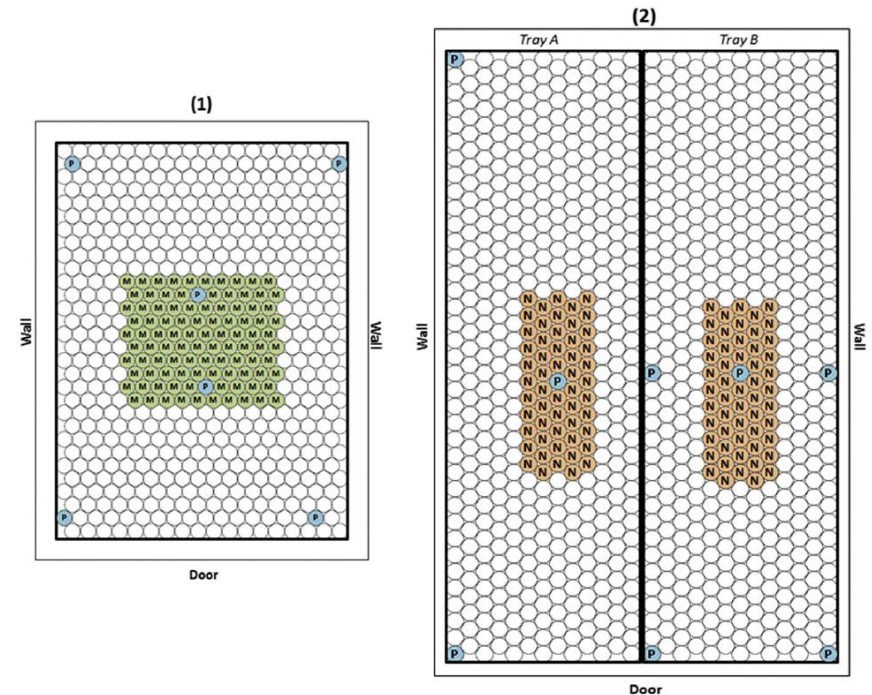


Figure 1. Vial arrangements in (1) LYO A and (2) LYO B. Gravimetrically analyzed vials are marked with the letters M and N for LYO A and B, respectively. Vials in which wireless temperature probes were located are marked with the letter P. All vials were filled with 1.8 mL of pure water.